# Vapor Pressures and Sublimation Enthalpies of Gadolinium Trichloride, Tribromide, and Triiodide and Terbium Trichloride, Tribromide, and Triiodide

# V. Piacente,\*,<sup>†</sup> P. Scardala,<sup>†</sup> and B. Brunetti<sup>‡</sup>

Dipartimento di Chimica and Istituto per lo Studio dei Materiali Nanostrutturati, CNR Dipartimento di Chimica, Università "La Sapienza", P.le A. Moro 5, 00185 Roma, Italy

The equilibrium vapor pressures over  $GdCl_3$ ,  $GdBr_3$ ,  $\alpha$ - $GdI_3$ ,  $TbCl_3$ ,  $TbBr_3$ , and  $\alpha$ - $TbI_3$  were measured by the torsion-effusion method. The obtained data are well represented in the covered temperature ranges by the following selected equations:

| GdCl <sub>3</sub> (l)          | $\log(p/kPa) = 9.50 \pm 0.30 - (13\ 113 \pm 300)(K/T)$ (from 930 to 1213 K)  |
|--------------------------------|--|
| GdBr <sub>3</sub> (s)          | $\log(p/kPa) = 11.46 \pm 0.20 - (14\ 355 \pm 200)(K/T)$ (from 895 to 1057 K) |
| GdBr <sub>3</sub> (l)          | $\log(p/kPa) = 9.75 \pm 0.30 - (12\ 671 \pm 400)(K/T)$ (from 1060 to 1179 K) |
| $\alpha$ -GdI <sub>3</sub> (s) | $\log(p/kPa) = 10.99 \pm 0.20 - (13\ 651 \pm 200)(K/T)$ (from 890 to 1012 K) |
| TbCl <sub>3</sub> (l)          | $\log(p/kPa) = 9.13 \pm 0.20 - (12\ 210 \pm 200)(K/T)$ (from 921 to 1117 K)  |
| TbBr <sub>3</sub> (s)          | $\log(p/kPa) = 11.09 \pm 0.20 - (14\ 013 \pm 200)(K/T)$ (from 904 to 1108 K) |
| $\alpha$ -TbI <sub>3</sub> (s) | $\log(p/kPa) = 11.33 \pm 0.30 - (13\ 850 \pm 400)(K/T)$ (from 861 to 1078 K) |
|                                |  |

Considering the vapor consists only of the monomeric form, by the second- and third-law treatment of the experimental data, the following standard sublimation enthalpies of the compounds were derived:  $\Delta_{sub}H^{\circ}(298 \text{ K}) = (311 \pm 4, 292 \pm 2, 279 \pm 2, 296 \pm 4, 288 \pm 4, and 279 \pm 2) \text{ kJ} \cdot \text{mol}^{-1}$  for GdCl<sub>3</sub>, GdBr<sub>3</sub>,  $\alpha$ -GdI<sub>3</sub>, TbCl<sub>3</sub>, TbCl<sub>3</sub>, TbBr<sub>3</sub>, and  $\alpha$ -TbI<sub>3</sub>, respectively.

## Introduction

This work is a continuation of our systematic study carried out in order to determine the sublimation enthalpies of rare-earth trihalides from measurements of their vapor pressures. The standard sublimation enthalpies determined in previous works<sup>1–7</sup> present an evident trend for the light lanthanides going from trichlorides to triiodides (La,<sup>1</sup> Ce,<sup>2</sup> Pr,<sup>3</sup> Nd,<sup>4</sup> and Sm<sup>5</sup>) while they are comparable for the corresponding trihalides of heavy lanthanides (Dy<sup>6</sup> and Ho<sup>7</sup>). In the present paper the results obtained from the study of gadolinium trihalides (GdCl<sub>3</sub>, GdBr<sub>3</sub>, and  $\alpha$ -GdI<sub>3</sub>) and of terbium trihalides (TbCl<sub>3</sub>, TbBr<sub>3</sub>, and  $\alpha$ -TbI<sub>3</sub>) are reported.

The vapor pressures for GdCl<sub>3</sub> and TbCl<sub>3</sub> were measured by Moriarty<sup>8</sup> and by Myers and Hannay<sup>9</sup> both by using the Knudsen effusion method and, at the highest temperatures, by Dudchik et al.<sup>10</sup> by using the boiling point method. Some Knudsen vapor pressure values for GdCl<sub>3</sub> were also measured by Evseeva and Zenkevich.<sup>11</sup> The sublimation enthalpy for this compound was mass-spectrometrically obtained by Ciach et al.<sup>12</sup> from the slope of a log I<sup>+</sup>*T* versus 1/*T* equation. Moreover, in the mass-spectrometric investigations of the vapor above TbCl<sub>3</sub>,<sup>13,14</sup> partial pressure

<sup>‡</sup> Istituto per lo Studio dei Materiali Nanostrutturati, CNR Dipartimento di Chimica. values of the monomeric (TbCl<sub>3</sub>), dimeric (Tb<sub>2</sub>Cl<sub>6</sub>), and trimeric (Tb<sub>3</sub>Cl<sub>9</sub>) forms were measured and the corresponding partial sublimation enthalpies were derived. As concerns GdBr<sub>3</sub> and TbBr<sub>3</sub>, the vapor pressures of both compounds were mass-spectrometrically measured by Gietmann et al.<sup>15</sup> and, at the highest temperatures, by Makhmadmurodov et al.<sup>16</sup> using the boiling point method. Also Weigel and Trinkl,<sup>17</sup> by using a particular static method, measured the vapor pressures of gadolinium triiodide and terbium triiodide reported in the literature are those measured by the Knudsen method by Hirayama et al.<sup>18,19</sup>

### **Experimental Section**

The samples of gadolinium and terbium trihalides used in this study were supplied by Aldrich and were 99.9% pure as certified by the supplier. To minimize oxidation and hydrolysis of the samples, the manipulations and loading of the torsion cells were carried out in a drybox. A drop of naphthalene was placed over the effusion holes of the cells to protect the sample during the transfer in the torsion assembly. The torsion apparatus employed in the present work for the measurements of vapor pressures was practically the same as that described in detail and used in our previous work.<sup>20</sup> Several conventional torsion cells with different materials and areas of their effusion holes (cell type A, stainless steel with both holes 0.5 mm in diameter,

<sup>\*</sup> Corresponding author. Phone: +3906490156. Fax: +390649913951. E-mail: vincenzo.piacente@uniromal.it. † Dipartimento di Chimica.

and cell type B, graphite with both holes 1.0 mm in diameter) were used. The molten compounds present creeping-out effects. To minimize this effect and possible interaction with the cell material and to increase the surface of the sample, the samples were put in a small molybdenum nest of close texture inserted in the lodgings of the cell. As in the previous works,<sup>4,5</sup> a particular stainless steel cell, cell C, having two effusion holes with different areas (0.6 and 1.9 mm in diameter, respectively) was also employed in the present work. By using this cell, the vapor pressures of a compound can be measured over a large temperature range in a single experiment. In fact, by filling both lodgings of this cell with the sample, in the first step of the experiment, the torsion of the tungsten wire to which the cell is suspended is due to the effusion of the vapor through both holes (cell  $C_1$ ). As the sample in the lodging with a large effusion hole vaporizes in a greater amount than that in the other one, when the sample in this lodging is completely vaporized, the torsion of the assembly decreases because it is due to the effusion of the vapor from the sample in the lodging with the smaller hole. This permits us to increase the temperature interval and to obtain vapor pressure values at the highest temperatures under the same experimental conditions of the first step of the measurement. Under these conditions the cell behaves as a new cell (cell C<sub>2</sub>). The two cell constants of this "double cell" (cell C1 and C2) necessary to convert the torsion angles to pressure values, as well as those of the other cells A and cells B, were determined by vaporizing a pure standard (lead) having a well-known vapor pressure.<sup>21</sup> These constants were checked during the experiments, and their values were found to be reproducible within about 15%. This uncertainty produces a displacement in the final log *p* values of about  $\pm 0.1$ . The displacement due to errors in the torsion angle measurements is negligible. The uncertainties associated with the temperature values, measured by a calibrated Pt-Pt/Rh (10% Rh) thermocouple inserted in a second cell placed just beneath the torsion one, are also negligible and in the entire temperature range should not exceed  $\pm 1$  K. To minimize systematic errors and as a check on equilibrium inside the cell, in the pressure measurement the temperatures were increased and decreased at random, although in the tables, for each run, the results are reported as increasing temperatures.

#### Results

Gadolinium Trihalides. The total vapor pressures measured in various runs above liquid GdCl<sub>3</sub>, GdBr<sub>3</sub> in both the solid and liquid phases (melting point at 1058 K<sup>22</sup>), and solid  $GdI_3$ , in both in the  $\alpha$  and  $\beta$  phases (transition at 1013 K<sup>23</sup>), are reported in Table 1 and Figure 1. In Figure 2 are reported the experimental torsion angles obtained by using cell C in the study of GdBr<sub>3</sub> (runs A1 and A2). Among all the vapor pressure data for GdBr<sub>3</sub> measured by this cell in the first step of each experiment (when both lodgings were full of sample, cell C<sub>1</sub>), the only values measured at temperatures lower than the melting point (mp =  $1058 \text{ K}^{22}$ ) above the solid compound were reported and taken into account in the evaluation of the sublimation enthalpy. Among all the vapor pressures measured in the second step of the experiments, using cell C as  $C_2$  (when the only lodging with the smaller hole was still full of sample), only those measured at temperatures higher than the melting point above the molten compound were taken into account. Equally, for α-GdI<sub>3</sub> in the experiments carried out with cell C as C1 and C2, only vapor pressures measured at temperatures lower and higher than the crystal transition (1013 K) above the  $\alpha$  and  $\beta$  solid

phases, respectively, were reported in Table 1 and Figure 1. For each run, the slope and intercept of the log *p* versus 1/T equation representative of the experimental data was obtained by the least-squares method. In Table 2 are reported the so obtained values with the corresponding standard deviations together with the covered temperature ranges. The slight inconsistencies among log p versus 1/Tequations could be due to unavailable small errors in the experimental torsion and temperature measurements, to errors associated with the cell constants of the different used cells, and to the expected failure of the least-squares treatment when applied both to a too small number of data points and over a small temperature range. Apparently no evident dependence of the pressure values on the area of the effusion holes of the used cells, and in particular of cell C, was observed. By weighting the slopes and intercepts reported in Table 2 proportionally to the corresponding numbers of experimental points, the following log *p* versus 1/T equations representative of the vapor pressures of gadolinium trihalides were selected:

$$GdCl_3(l)$$

$$log(p/kPa) = 9.50 \pm 0.30 - (13\ 113 \pm 300)(K/T)$$
  
(from 930 to 1213 K) (1)

 $GdBr_3(s)$ 

$$\log(p/kPa) = 11.46 \pm 0.20 - (14\ 355 \pm 200)(K/T)$$
  
(from 895 to 1057 K) (2)

 $GdBr_3(l)$ 

$$log(p/kPa) = 9.75 \pm 0.30 - (12\ 671 \pm 400)(K/T)$$
  
(from 1060 to 1179 K) (3)

 $\alpha$ -GdI<sub>3</sub>(s)

$$\log(p/kPa) = 11.99 \pm 0.20 - (13651 \pm 200)(K/T)$$
  
(from 890 to 1012 K) (4)

where the associated errors were estimated. As concerns GdI<sub>3</sub>, because the number of experimental points obtained by cell C used as  $C_2$  above the  $\beta$  phase is small, the errors associated with slopes and intercepts of the corresponding log *p* versus 1/T equations are decidedly larger than those calculated as standard deviations, so that a final equation representative of the vapor pressure of  $\beta$ -GdI<sub>3</sub> was not selected as reliable. The vapor pressure values measured by cell  $C_2$  above  $\beta$ -GdI<sub>3</sub> were only taken as a check that not large errors should have been made in the pressure measured above  $\alpha$ -GdI<sub>3</sub> by using cell B and cell C as C<sub>1</sub>. As concerns GdBr<sub>3</sub>, from the log *p* versus 1/T equations obtained above solid and liquid phases (run A, D, and G in Table 4) and from the selected ones (eqs 2 and 3), rough values of the enthalpy of fusion and of the melting point of this compound were calculated and reported in Table 3 together with the corresponding calorimetric values obtained by Dworkin and Bredig.<sup>22</sup> Considering the procedure for melting point calculation, the errors associated with their values are difficult to evaluate because they are connected with the uncertainties of the slope and intercept of the log p versus 1/T equation and mainly with those of the cell constants of the used cell C. In any case, they are decidedly very large but the obtained data are important because they show that not large errors should have been made in the absolute temperature measurements.

**Terbium Trihalides.** The experimental total vapor pressures over liquid TbCl<sub>3</sub>, solid TbBr<sub>3</sub>, and solid  $\alpha$ -TbI<sub>3</sub> are reported in Table 4 and in Figure 3. By treating the

Table 1. Total Vapor Pressures Measured by the Torsion Method above  $GdX_3$  (X = Cl, Br, I)

|  |   |   |  |   | Ge  | dCl <sub>3</sub>  |   |  |  |  |   |
|--|---|---|--|---|---|---|---|--|--|--|---|
| run  | A (cell B)  | rur   | n B1 (cell C <sub>1</sub> )  | run   | B2 (cell C <sub>2</sub> )   | run D   | 1 (cell C <sub>1</sub> )  | run D2   | 2 (cell C <sub>2</sub> )   | ru   | n E (cell A)  |
| <i>T</i> /K  | -log(p/kPa)   | <i>T</i> /K   | −log(p/kI  | Pa) 7/K   | -log(p/kPa)   | <i>T</i> /K   | -log(p/kPa)   | <i>T</i> /K  | -log(p/kPa)  | <i>T</i> /K  | -log(p/kPa)   |
| 958<br>965<br>973<br>983<br>994<br>1004<br>1015<br>1024  | $\begin{array}{c} 4.20 \\ 4.11 \\ 4.01 \\ 3.85 \\ 3.71 \\ 3.60 \\ 3.45 \\ 3.31 \end{array}$   | 930<br>952<br>957<br>970<br>983<br>1002<br>1022<br>1046<br>1054 | 4.48<br>4.17<br>4.08<br>3.89<br>3.75<br>3.49<br>3.25<br>3.00<br>2.85                           | $1044\\1061\\1076\\1086\\1091\\1103\\1113\\1117\\1126\\1138\\1147\\1156\\1170\\1187$  | 3.00<br>2.87<br>2.66<br>2.57<br>2.47<br>2.36<br>2.24<br>2.22<br>2.12<br>2.01<br>1.89<br>1.80<br>1.66<br>1.49        | 996<br>1011<br>1023<br>1042<br>1052<br>1062<br>1071<br>1082<br>1090   | 3.65<br>3.48<br>3.32<br>3.10<br>2.99<br>2.86<br>2.76<br>2.63<br>2.56  | 1099<br>1107<br>1116<br>1120<br>1126<br>1135<br>1144<br>1154   | 2.47<br>2.38<br>2.29<br>2.23<br>2.18<br>2.10<br>2.00<br>1.88   | 1093<br>1107<br>1120<br>1134<br>1151<br>1165<br>1177<br>1190<br>1203<br>1213                     | $\begin{array}{c} 2.52\\ 2.38\\ 2.22\\ 2.06\\ 1.90\\ 1.74\\ 1.62\\ 1.50\\ 1.39\\ 1.30\end{array}$                             |
|  |   |   |  |   | Go  | dBr <sub>3</sub>  |   |  |  |  |   |
| ru   | $n A1 (cell C_1)$   |   | run A2   | $(\text{cell } C_2)$  | run B   | (cell B)  |   | un C (cell B)  |  | run D  | $\frac{1 \text{ (cell C}_1)}{1 \text{ (cell C}_1)}$   |
| 7/K  | -log(p/kPa)   |   | 7/K  | -log(p/kPa)   | 7/K   | -log(p/kPa)   | ) 7/K   | -log(p   | /kPa)  | 7/K  | -log(p/kPa)   |
| 893<br>917<br>926<br>937<br>947<br>957<br>967<br>980<br>980<br>987<br>990<br>997<br>1001<br>1011<br>1014<br>1020<br>1029 | $\begin{array}{c} 4.46\\ 4.11\\ 3.95\\ 3.78\\ 3.63\\ 3.48\\ 3.33\\ 3.12\\ 3.00\\ 2.97\\ 2.84\\ 2.81\\ 2.66\\ 2.61\\ 2.54\\ 2.43\end{array}$ |   | 1073<br>1073<br>1085<br>1096<br>1105<br>1114<br>1123<br>1140<br>1148<br>1148                   | 2.19<br>2.07<br>1.93<br>1.80<br>1.69<br>1.62<br>1.55<br>1.37<br>1.29<br>1.21  | 910<br>928<br>945<br>957<br>968<br>979<br>984<br>989<br>999<br>1008<br>1015<br>1018<br>1023<br>1029<br>1032<br>1035 | 4.38<br>4.11<br>3.81<br>3.65<br>3.49<br>3.33<br>3.25<br>3.15<br>2.99<br>2.85<br>2.77<br>2.66<br>2.56<br>2.53<br>2.47  | $\begin{array}{c} 931\\ 959\\ 965\\ 969\\ 973\\ 979\\ 983\\ 988\\ 993\\ 1000\\ 1004\\ 1011\\ 1014\\ 1019\\ 1025\\ 1030\\ 1041\\ 1045\\ 1049\end{array}$ | 3.6<br>3.4<br>3.4<br>3.3<br>3.2<br>3.1<br>3.1<br>3.1<br>3.1<br>2.8<br>2.8<br>2.8<br>2.6<br>2.6<br>2.6<br>2.6<br>2.6<br>2.6<br>2.6<br>2.6<br>2.6<br>2.6 | 50<br>19<br>19<br>10<br>26<br>27<br>10<br>26<br>26<br>27<br>26<br>30<br>30<br>30<br>30<br>30<br>30<br>30<br>30<br>30<br>30 | 968<br>968<br>979<br>990<br>1002<br>1014<br>1026<br>1041<br>1049<br>1057                         | 3.85<br>3.55<br>3.37<br>3.21<br>3.04<br>2.87<br>2.70<br>2.50<br>2.38<br>2.28  |
| ru   | n D2 (cell C <sub>2</sub> )   |   | run E (  | (cell B)  | run F   | (cell B)  | ru  | n G1 (cell C   | 1)   | run G  | 2 (cell C <sub>2</sub> )  |
| <i>T</i> /K  | -log(p/kPa)   |   | <i>T</i> /K  | -log(p/kPa)   | <i>T</i> /K   | -log(p/kPa)   | <i>T</i> /K   | -log(p   | v/kPa)   | <i>T</i> /K  | -log(p/kPa)   |
| $\begin{array}{r} 1074\\ 1091\\ 1099\\ 1108\\ 1119\\ 1130\\ 1140\\ 1150\\ 1159\\ 1168\\ 1179 \end{array}$                | $2.13 \\ 1.94 \\ 1.86 \\ 1.75 \\ 1.64 \\ 1.52 \\ 1.42 \\ 1.31 \\ 1.23 \\ 1.15 \\ 1.04$  |   | 914<br>929<br>941<br>956<br>971<br>994<br>1003<br>1012<br>1023<br>1032<br>1043<br>1051<br>1057 | $\begin{array}{c} 4.20\\ 3.98\\ 3.77\\ 3.55\\ 3.31\\ 3.15\\ 2.96\\ 2.83\\ 2.71\\ 2.56\\ 2.43\\ 2.29\\ 2.18\\ 2.11\end{array}$ | 920<br>934<br>945<br>956<br>964<br>974<br>986<br>996<br>1006<br>1015<br>1025<br>1034<br>1043<br>1051<br>1057<br>G   | 4.11<br>3.87<br>3.69<br>3.52<br>3.40<br>3.26<br>3.05<br>2.91<br>2.79<br>2.66<br>2.52<br>2.40<br>2.29<br>2.29<br>2.29<br>2.29<br>2.29<br>2.29<br>2.29<br>2.2 | $\begin{array}{c} 919\\ 932\\ 953\\ 962\\ 969\\ 977\\ 990\\ 999\\ 1008\\ 1018\\ 1026\\ 1036\\ \end{array}$  | 4.0<br>3.8<br>3.4<br>3.3<br>3.2<br>3.1<br>2.5<br>2.7<br>2.5<br>2.4<br>2.3  | 05<br>36<br>49<br>35<br>24<br>22<br>24<br>31<br>70<br>56<br>56<br>33   | 1067<br>1078<br>1087<br>1098<br>1108<br>1119<br>1128<br>1138<br>1138<br>1150<br>1161<br>1169     | $\begin{array}{c} 2.03 \\ 1.92 \\ 1.84 \\ 1.72 \\ 1.63 \\ 1.52 \\ 1.43 \\ 1.33 \\ 1.21 \\ 1.10 \\ 1.04 \end{array}$           |
| ru   | n A (cell B)  |   | run B1 (   | cell C <sub>1</sub> )   | run B2  | (cell C <sub>2</sub> )  | ru  | in C (cell B)  |  | run E  | (cell B)  |
| <i>T</i> /K  | -log(p/kPa)   |   | 77K -  | -log(p/kPa)   | <i>T</i> /K   | -log(p/kPa)   | <i>T</i> /K   | -log(p   | /kPa)  | <i>T</i> /K  | -log(p/kPa)   |
| 913<br>925<br>934<br>952<br>952<br>962<br>974<br>983<br>992  | 3.95<br>3.75<br>3.57<br>3.46<br>3.31<br>3.15<br>2.99<br>2.87<br>2.76  | 1   | 914<br>924<br>928<br>936<br>943<br>951<br>959<br>966<br>978<br>9988<br>997<br>1006             | 4.05<br>3.91<br>3.84<br>3.70<br>3.61<br>3.48<br>3.35<br>3.24<br>3.08<br>2.94<br>2.86<br>2.72                                  | 1023<br>1033<br>1045<br>1055<br>1064<br>1074<br>1083<br>1094<br>1102  | $\begin{array}{c} 2.17\\ 2.06\\ 1.90\\ 1.77\\ 1.66\\ 1.52\\ 1.40\\ 1.27\\ 1.17\end{array}$  | $905 \\ 918 \\ 928 \\ 939 \\ 947 \\ 957 \\ 966 \\ 975 \\ 984 \\ 993 \\ 1002 \\ 1011$  | 4.0<br>3.8<br>3.7<br>3.5<br>3.4<br>3.2<br>3.1<br>2.9<br>2.8<br>2.7<br>2.6<br>2.4   | 97<br>77<br>73<br>11<br>53<br>11<br>54<br>00<br>97<br>74<br>44<br>50<br>88   | 891<br>911<br>919<br>928<br>937<br>944<br>955<br>962<br>970<br>979<br>987<br>995<br>1003<br>1012 | $\begin{array}{c} 4.25\\ 3.95\\ 3.81\\ 3.68\\ 3.55\\ 3.45\\ 3.28\\ 3.15\\ 3.04\\ 2.90\\ 2.79\\ 2.67\\ 2.57\\ 2.45\end{array}$ |
| ru   | n E1 (cell C <sub>1</sub> )   |   | run E2   | (cell C <sub>2</sub> )  | run Fi  | (cell C <sub>1</sub> )  | ru  | ın F2 (cell C  | C <sub>2</sub> )   | run (  | G (cell B)  |
| <i>T</i> /K  | -log(p/kPa)   |   | <i>T</i> /K  | -log(p/kPa)   | <i>T</i> /K   | -log(p/kPa  | .) <i>T</i> /K  | -log(  | p/kPa)   | <i>T</i> /K  | -log(p/kPa)   |
| 890<br>901<br>916<br>927<br>937<br>948<br>957<br>967<br>978<br>990<br>1002<br>1011                                       | $\begin{array}{r} 4.35\\ 4.17\\ 3.95\\ 3.76\\ 3.60\\ 3.43\\ 3.34\\ 3.14\\ 2.97\\ 2.81\\ 2.66\\ 2.55\end{array}$                             |   | 1019<br>1026<br>1040<br>1052<br>1066<br>1082   | 2.47<br>2.39<br>2.22<br>2.06<br>1.87<br>1.67  | 901<br>914<br>922<br>929<br>938<br>946<br>955<br>964<br>973<br>985<br>993<br>1002                                   | $\begin{array}{r} 4.08\\ 3.86\\ 3.75\\ 3.63\\ 3.49\\ 3.40\\ 3.22\\ 3.10\\ 2.97\\ 2.80\\ 2.69\\ 2.60\end{array}$   | $\begin{array}{c} 1021\\ 1033\\ 1042\\ 1054\\ 1066\\ 1076\\ 1086\\ 1097\\ \end{array}$  | 2.<br>2.<br>2.<br>2.<br>1.<br>1.<br>1.   | 41<br>27<br>16<br>01<br>84<br>68<br>55<br>43   | 901<br>912<br>920<br>927<br>933<br>942<br>954<br>966<br>975<br>983<br>992                        | 4.25<br>4.05<br>3.95<br>3.82<br>3.72<br>3.57<br>3.38<br>3.20<br>3.05<br>2.94<br>2.85  |



**Figure 1.** Experimental vapor pressure of  $GdCl_3$  (a),  $GdBr_3$  (b), and  $\alpha$ -GdI<sub>3</sub> (c) measured by the torsion method.

experimental data as for gadolinium trihalides, the log p versus 1/T equations representative of the vapor pressures of these compounds measured in each run were calculated and reported in Table 5. From these the following final equations were derived:

 $\text{TbCl}_3(\mathbf{l})$ 

$$log(p/kPa) = 9.13 \pm 0.20 - (12210 \pm 200)(K/T)$$
(from 921 to 1117 K) (5)

 $TbBr_3(s)$ 

 $log(p/kPa) = 11.09 \pm 0.20 - (14013 \pm 200)(K/T)$ (from 904 to 1108 K) (6)

$$\alpha$$
-TbI<sub>3</sub>(s)  
log(p/kPa) = 11.33 ± 0.30 - (13850 ± 400)(K/T)  
(from 861 to 1078 K) (7)

where all the quoted errors were estimated.

## Discussion

The pressure dependences of the vapor pressures of gadolinium and terbium trihalides measured in the present work are well represented by the selected log p versus 1/T equations (eqs 1–7). These equations are reported in Table 6 and in Figures 4 and 5 together with those found in the

Table 2. Temperature Dependence of the Total Vapor Pressure of  $GdX_3$  (X = Cl, Br, I)

|                                |       |     | no. of | $\Delta T$  | $\log(p/kPa) =$  | A - B/(T/K)      |
|--------------------------------|-------|-----|--------|-------------|------------------|------------------|
| compd                          | cell  | run | points | К           | $A^a$            | $B^a$            |
| GdCl <sub>3</sub> (l)          | В     | А   | 8      | 958-1024    | $9.41 \pm 0.19$  | $13~041\pm187$   |
| GdCl <sub>3</sub> (l)          | $C_1$ | B1  | 9      | 930-1054    | $9.09\pm0.15$    | $12\ 608\pm151$  |
| GdCl <sub>3</sub> (l)          | $C_2$ | B2  | 14     | 1044-1187   | $9.69\pm0.15$    | $13\ 293\pm170$  |
| GdCl <sub>3</sub> (l)          | $C_1$ | D1  | 9      | 996-1090    | $9.12\pm0.08$    | $12\ 728\pm87$   |
| GdCl <sub>3</sub> (l)          | $C_2$ | D2  | 8      | 1099 - 1154 | $9.59 \pm 0.26$  | $13\ 251\pm 287$ |
| GdCl <sub>3</sub> (l)          | Α     | Ε   | 10     | 1093-1213   | $9.93 \pm 0.09$  | $13\ 612\pm 105$ |
| GdBr <sub>3</sub> (s)          | $C_1$ | A1  | 16     | 895-1029    | $11.42\pm0.08$   | $14\ 238\pm79$   |
| GdBr <sub>3</sub> (l)          | $C_2$ | A2  | 10     | 1060 - 1155 | $9.71\pm0.14$    | $12\ 626\pm158$  |
| GdBr <sub>3</sub> (s)          | В     | В   | 16     | 910-1035    | $11.50\pm0.14$   | $14\;480\pm139$  |
| GdBr <sub>3</sub> (s)          | В     | С   | 19     | 951-1049    | $11.62\pm0.07$   | $14\;484\pm66$   |
| GdBr <sub>3</sub> (s)          | $C_1$ | D1  | 10     | 951-1057    | $11.63\pm0.10$   | $14~698\pm101$   |
| GdBr <sub>3</sub> (l)          | $C_2$ | D2  | 11     | 1074-1179   | $10.13\pm0.06$   | $13\ 166\pm 62$  |
| GdBr <sub>3</sub> (s)          | В     | Ε   | 14     | 914-1057    | $11.41\pm0.05$   | $14\ 287\pm52$   |
| GdBr <sub>3</sub> (s)          | В     | F   | 15     | 920-1057    | $11.41\pm0.05$   | $14\ 272\pm 50$  |
| GdBr <sub>3</sub> (s)          | $C_1$ | G1  | 12     | 919-1036    | $11.23\pm0.10$   | $14~035\pm98$    |
| GdBr <sub>3</sub> (l)          | $C_2$ | G2  | 11     | 1067 - 1169 | $9.41\pm0.11$    | $12\ 215\pm118$  |
| $\alpha$ -GdI <sub>3</sub> (s) | В     | Α   | 9      | 913-992     | $11.02\pm0.21$   | $13~654\pm201$   |
| $\alpha$ -GdI <sub>3</sub> (s) | $C_1$ | B1  | 12     | 914-1006    | $10.66\pm0.14$   | $13\;443\pm138$  |
| $\beta$ -GdI <sub>3</sub> (s)  | $C_2$ | B2  | 9      | 1023-1102   | $11.94\pm0.15$   | $14\ 454\pm 164$ |
| $\alpha$ -GdI <sub>3</sub> (s) | В     | С   | 12     | 905-1011    | $11.27\pm0.06$   | $13\ 892\pm 62$  |
| $\alpha$ -GdI <sub>3</sub> (s) | В     | D   | 14     | 891-1012    | $10.98 \pm 0.11$ | $13~598\pm109$   |
| $\alpha$ -GdI <sub>3</sub> (s) | $C_1$ | E1  | 12     | 890-1011    | $10.90\pm0.13$   | $13~590\pm125$   |
| $\beta$ -GdI <sub>3</sub> (s)  | $C_2$ | E2  | 6      | 1019-1082   | $11.37\pm0.20$   | $14\ 116\pm 205$ |
| $\alpha$ -GdI <sub>3</sub> (s) | $C_1$ | F1  | 12     | 901-1002    | $10.79\pm0.12$   | $13~392\pm118$   |
| $\beta$ -GdI <sub>3</sub> (s)  | $C_2$ | F2  | 8      | 1021-1097   | $12.08 \pm 0.32$ | $14\ 824\pm 343$ |
| $\alpha$ -GdI <sub>3</sub> (s) | B     | G   | 11     | 901-992     | $11.32\pm0.15$   | $14~028\pm138$   |
|                                |       |     |        |             |                  |                  |

<sup>a</sup> The quoted errors are standard deviations.

Table 3. Melting Point and Enthalpy of Fusion for GdBr<sub>3</sub>

|                                  | $\Delta_{ m fus}H^{\circ}$ | $T_{ m fus}$ |
|----------------------------------|----------------------------|--------------|
| source                           | kJ∙mol <sup>−1</sup>       | K            |
| runs $A_1$ and $A_2$             | $31\pm4$                   | 943          |
| runs $D_1$ and $D_2$             | $29\pm3$                   | 1022         |
| runs $G_1$ and $G_2$             | $35\pm4$                   | 999          |
| eqs 2 and 3                      | $32\pm11$                  | 982          |
| Dworkin and Bredig <sup>22</sup> | 38                         | 1058         |



**Figure 2.** Experimental torsion angles measured over  $GdBr_3$  by cell C in the A1 and A2 runs.

literature. In general our pressure data, within the errors limits, are not in conflict with the reference data. Only for  $\alpha$ -GdI<sub>3</sub>, although the absolute pressure values are comparable, is the slope of our final equation lower than that reported by Hirayama et al.<sup>19</sup>

As in the covered temperature ranges the amount of the dimer form in the gaseous phase above all the studied compounds was considered negligible compared to that of the monomer form, the measured total vapor pressures were considered partial pressures of the corresponding monomers. In this way, the second-law sublimation or vaporization enthalpies of the studied trihalides in monomeric form were calculated, at the middle experimental

Table 4. Total Vapor Pressures Measured by the Torsion Method above  $TbX_3$  (X = Cl, Br, I)

 $TbCl_{3} \\$ 

| run   | A (cell B)   | ru          | n B (cell  | l B)   | run   | C (cell A)   | run  | E (cell B)  | rur               | n F (cell A)  | rur   | n H (cell A)   |
|---|--|-------------|--|--|---|--|--|---|-------------------|---|---|--|
| <i>T</i> /K   | -log(p/kPa)  | <i>T</i> /K | -log(  | <i>p</i> /kPa)   | <i>T</i> /K   | -log(p/kPa)  | <i>T</i> /K  | -log(p/kPa)   | <i>T</i> /K       | -log(p/kPa)   | <i>T</i> /K   | -log(p/kPa)  |
| 942   | 3.68   | 946         | 3.   | .78  | 979   | 3.35   | 921  | 4.17  | 979               | 3.48  | 976   | 3.48   |
| 957   | 3.48   | 957         | 3.   | 61   | 994   | 3.15   | 931  | 4.00  | 995               | 3.30  | 992   | 3.30   |
| 971   | 3.30   | 967         | 3.   | 48   | 998   | 3.10   | 937  | 3.87  | 1009              | 3.13  | 1006  | 3.13   |
| 988   | 3.08   | 980         | 3.   | .30  | 1010  | 2.94   | 943  | 3.77  | 1017              | 3.04  | 1017  | 3.00   |
| 999   | 2.97   | 990         | 3.<br>3  | .18  | 1017  | 2.88   | 950  | 3.69  | 1028              | 2.91  | 1027  | 2.91   |
| 1021  | 2.72   | 1010        | 3.<br>2.   | .04  | 1020  | 2.67   | 953<br>961   | 3.54  | 1033              | 2.72  | 1037  | 2.68   |
| 1033  | 2.59   | 1020        | 2.   | .80  | 1043  | 2.58   | 965  | 3.52  | 1054              | 2.61  | 1058  | 2.58   |
| 1045  | 2.45   | 1029        | 2.   | .68  | 1054  | 2.45   | 971  | 3.43  | 1067              | 2.43  | 1071  | 2.43   |
| 1053  | 2.35   | 1038        | 2.   | .59  | 1056  | 2.43   | 975  | 3.39  |                   |   | 1082  | 2.27   |
| 1064  | 2.24   | 1047        | 2.   | .48  | 1059  | 2.41   | 984  | 3.27  |                   |   | 1093  | 2.15   |
| 1071  | 2.17   | 1057        | ۵.<br>2  | .38<br>29  | 1072  | 2.28   | 994<br>1006  | 3.13<br>2.08  |                   |   | 1105  | 2.04   |
| 1092  | 1.95   | 1075        | 2.   | .21  | 1091  | 2.07   | 1017   | 2.87  |                   |   | 1117  | 1.55   |
| 1102  | 1.85   |             |  |  |   |  | 1024   | 2.78  |                   |   |   |  |
|   |  |             |  |  |   |  | 1037   | 2.60  |                   |   |   |  |
|   |  |             |  |  |   | Th   | Bra  |   |                   |   |   |  |
|   | A (aall A)   |             | D (aa)   | 11 A)  |   |  |  | D (call D)  |                   |   |   | E1 (call C)  |
| run   | A (cell A)   | ru          | IN B (cel  | II A)  | ru  | n C (cell B)   | run  | D (cell B)  | rui               | 1 E (cell A)  | - run   | F1 (cell $C_1$ )   |
| <i>T</i> /K   | -log(p/kPa)  | <i>T</i> /K | -log   | (p/kPa)  | <i>T</i> /K   | -log(p/kPa)  | <i>T</i> /K  | -log(p/kPa)   | <i>T</i> /K       | -log(p/kPa  | ) <i>T</i> /K   | -log(p/kPa)  |
| 957   | 3.48   | 922         | 4  | 1.08   | 904   | 4.32   | 915  | 4.32  | 920               | 4.08  | 915   | 4.38   |
| 970   | 3.30   | 940         | 3  | 3.68   | 915   | 4.12   | 922  | 4.21  | 940               | 3.78  | 925   | 4.14   |
| 993   | 2.97   | 958         | 3  | 3.48   | 920   | 4.07   | 930  | 4.07  | 958               | 3.54  | 933   | 4.02   |
| 1004  | 2.83   | 9/4         | 3  | 5.24<br>0 07   | 924   | 3.98   | 937  | 3.91  | 976               | 3.30  | 940   | 3.92   |
| 1015  | 2.58   | 1004        | 2  | 2.80   | 935   | 3.80   | 943<br>950   | 3 74  | 1004              | 2.89  | 950<br>957  | 3.64   |
| 1035  | 2.48   | 1015        | 2  | 2.65   | 940   | 3.74   | 956  | 3.64  | 1014              | 2.78  | 964   | 3.54   |
| 1047  | 2.24   | 1025        | 2  | 2.53   | 944   | 3.68   | 962  | 3.56  | 1024              | 2.62  | 971   | 3.45   |
| 1059  | 2.07   | 1035        | 2  | 2.38   | 948   | 3.62   | 969  | 3.44  | 1032              | 2.53  | 977   | 3.37   |
| 1068  | 1.96   | 1042        | 2  | 2.27   | 954   | 3.53   | 975  | 3.37  | 1045              | 2.33  | 983   | 3.27   |
| 1070  | 1.65   | 1051        | 2  | 2.17   | 900   | 3.44   |  |   | 1054              | 2.19  |   |  |
| 1099  | 1.64   | 1068        | 1  | 1.94   |   |  |  |   | 1071              | 1.95  |   |  |
| 1108  | 1.54   | 1076        | 1  | .85  |   |  |  |   | 1078              | 1.85  |   |  |
|   |  | 1085        | 1  | 1.74   |   |  |  |   |                   |   |   |  |
|   |  |             |  |  |   |  |  |   |                   |   |   |  |
| ru  | n F2 (cell C <sub>2</sub>  |             | rui  | n G (cell  | A)  | run H  | (cell B)   | 1   | un I (cel         | l B)  | run l   | L (cell B)   |
| ru  | n F2 (cell C <sub>2</sub><br>$-\log(p/kP)$   | <br>a)      | rui<br><i>T</i> /K   | n G (cell<br>–log  | A) $(p/kPa)$  | run H  | (cell B)<br>-log( <i>p</i> /kF   | $ran \frac{r}{T/K}$   | un I (cel<br>—lo  | l B)<br>g(p/kPa)  | run l   | L (cell B)<br>$-\log(p/kPa)$   |
| ru  | $\frac{1}{-\log(p/kP)}$  | a)          | rui<br><i>T</i> /K   | n G (cell<br>–loge   | A)<br>(p/kPa)   | run H<br>7/K   | (cell B)<br>-log( <i>p</i> /kF   | Pa) 77K   | run I (cel<br>—lo | l B)<br>g( <i>p</i> /kPa)   | run l<br><i>T/</i> K  | L (cell B)<br>-log(p/kPa)  |
| <br>  | $\frac{1}{10000000000000000000000000000000000$   | a)          | rui<br><i>T</i> /K<br>928<br>937   | n G (cell<br>–loge<br>4<br>3   | A)<br>(p/kPa)<br>.02  | run H<br>77K<br>912<br>920   | (cell B)<br>-log( <i>p</i> /kF<br>4.42<br>4.32   | Pa)   | run I (cel<br>—lo | l B)<br>g(p/kPa)<br>4.33<br>4.09  | run l<br>7/K<br>921<br>934  | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92  |
| <br>  | n F2 (cell C <sub>2</sub><br>-log(p/kP<br>3.43<br>3.27<br>3.13   | a)          | rui<br><i>T</i> /K<br>928<br>937<br>944  | n G (cell<br>—logi<br>4<br>3<br>3  | A)<br>(p/kPa)<br>.02<br>.86<br>.73  | run H<br>7/K<br>912<br>920<br>934  | (cell B)<br>-log(p/kF<br>4.42<br>4.32<br>4.07  | Pa)   | run I (cel<br>—lo | l B)<br>g(p/kPa)<br>4.33<br>4.09<br>3.92  | run l<br>7/K<br>921<br>934<br>939   | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82  |
| <br>77K<br>962<br>973<br>983<br>993   | $ \frac{1}{10000000000000000000000000000000000$  | a)          | run<br>7/K<br>928<br>937<br>944<br>957   | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56   | run H<br>77K<br>912<br>920<br>934<br>941   | (cell B)<br>-log(p/kH<br>4.42<br>4.32<br>4.07<br>3.94  | Pa) 77K<br>908<br>917<br>931<br>947   | run I (cel<br>—lo | l B)<br>g(p/kPa)<br>4.33<br>4.09<br>3.92<br>3.67  | run 1<br>7/K<br>921<br>934<br>939<br>945  | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73  |
| 77K<br>962<br>973<br>983<br>993<br>1002   | $ \begin{array}{r} \text{m F2 (cell C_2} \\ \hline -\log(p/\text{kP}) \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.88 \\ 2.88 \end{array} $  | a)          | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>957   | n G (cell<br>-logy<br>4<br>3<br>3<br>3<br>3<br>3   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50  | run H<br>77K<br>912<br>920<br>934<br>941<br>948  | (cell B)<br>-log(p/kH<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.55<br>5.5                     | Pa)<br>77K<br>908<br>917<br>931<br>947<br>962<br>977  | run I (cel<br>—lo | l B)<br>g(p/kPa)<br>4.33<br>4.09<br>3.92<br>3.67<br>3.46  | run l<br>7/K<br>921<br>934<br>939<br>945<br>955   | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.57  |
| 77K<br>962<br>973<br>983<br>993<br>1002<br>1012   | $ \begin{array}{c} \text{m F2 (cell C_2} \\ \hline -\log(p/\text{kP}) \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.85 \end{array} $  | a)          | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988  | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>2  | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>06   | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962  | (cell B)<br>-log(p/kF<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>2.62  | Pa)<br>77K<br>908<br>917<br>931<br>947<br>962<br>978<br>901   | run I (cel<br>—lo | l B)<br>g(p/kPa)<br>4.33<br>4.09<br>3.92<br>3.67<br>3.46<br>3.21<br>2.00  | run l<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>072   | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>2.20  |
| 77K<br>962<br>973<br>983<br>993<br>1002<br>1012<br>1020<br>1030   | $ \begin{array}{r} \text{m F2 (cell C_2} \\ \hline -\log(p/\text{kP}) \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \end{array} $  | a)          | run<br>7/K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000  | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>2  | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90   | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968   | (cell B)<br>-log(p/kF<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53  | Image: Pa)         Image: T/K           908         917           931         947           962         978           991         1003  | run I (cel<br>—lo | I B)<br>g(p/kPa)<br>4.33<br>4.09<br>3.92<br>3.67<br>3.46<br>3.21<br>3.00<br>2.86  | run 1<br>7/K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981  | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18  |
| 77K<br>962<br>973<br>983<br>993<br>1002<br>1012<br>1020<br>1030<br>1039   | $ \begin{array}{r} \text{m F2 (cell C_2} \\ \hline -\log(p/\text{kP}) \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \\ 2.40 \end{array} $  | a)          | run<br>7/K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007  | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>2   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>962<br>968<br>974   | (cell B)<br>-log(p/kF<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45  | Image: Pa)         Image: T/K           908         917           931         947           962         978           991         1003           1014         104   | run I (cel<br>—lo | I B)<br>g(p/kPa)<br>4.33<br>4.09<br>3.92<br>3.67<br>3.46<br>3.21<br>3.00<br>2.86<br>2.68  | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990   | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04  |
| <u>ти</u><br><u>77К</u><br>962<br>973<br>983<br>993<br>1002<br>1012<br>1020<br>1030<br>1039<br>1049   | $ \begin{array}{r} \text{m F2 (cell C_2} \\ \hline -\log(p/\text{kP}) \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \\ 2.53 \\ 2.40 \\ 2.24 \end{array} $  | <br>a)      | run<br>7/K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007  | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>2   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980   | (cell B)<br>-log(p/kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.62<br>3.53<br>3.45<br>3.37  | $\begin{array}{c} & & & \\ \hline p_{a} & & \\ \hline \hline T/K \\ & & \\ 908 \\ 917 \\ 931 \\ 947 \\ 962 \\ 978 \\ 991 \\ 1003 \\ 1014 \\ 1019 \end{array}$   | run I (cel<br>—lo | I B)<br>g(p/kPa)<br>4.33<br>4.09<br>3.92<br>3.67<br>3.46<br>3.21<br>3.00<br>2.86<br>2.68<br>2.59  | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999  | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94  |
| ru           77K           962           973           983           993           1002           1012           1020           1030           1039           1049  | $ \begin{array}{r} \text{m F2 (cell C_2} \\ \hline -\log(p/\text{kP}) \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.65 \\ 2.53 \\ 2.40 \\ 2.24 \\ 2.15 \\ 2.15 \\ \end{array} $   | a)          | run<br>7/K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007  | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>2   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980   | (cell B)<br>-log(p/kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.62<br>3.45<br>3.37  | $\begin{array}{c} & & \\ \hline p_{a} & & \\ \hline \hline T/K \\ & 908 \\ 917 \\ 931 \\ 947 \\ 962 \\ 978 \\ 991 \\ 1003 \\ 1014 \\ 1019 \end{array}$  | run I (cel<br>—lo | 1 B)<br>g(p/kPa)<br>4.33<br>4.09<br>3.92<br>3.67<br>3.46<br>3.21<br>3.00<br>2.86<br>2.68<br>2.59  | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999  | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94  |
| ru           77K           962           973           983           993           1002           1012           1020           1030           1039           1049           1058           10676   | $ \begin{array}{r} \text{m F2 (cell } C_2 \\ \hline -\log(p/\text{kP}) \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.65 \\ 2.53 \\ 2.40 \\ 2.24 \\ 2.15 \\ 2.00 \\ 1.80 \\$ | a)          | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007  | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>2   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980   | (cell B)<br>-log(p/kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.62<br>3.45<br>3.37  | Image: Paper definition         Image: Paper definition           908         917           931         947           962         978           991         1003           1014         1019  | run I (cel<br>—lo | l B)<br>g(p/kPa)<br>4.33<br>4.09<br>3.92<br>3.67<br>3.46<br>3.21<br>3.00<br>2.86<br>2.68<br>2.59  | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999  | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94  |
| ru           77K           962           973           983           993           1002           1012           1020           1030           1039           1049           1058           1067           1088   | $\begin{array}{r} \text{m F2 (cell } C_2 \\ \hline -\log(p/\text{kP}) \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \\ 2.40 \\ 2.24 \\ 2.15 \\ 2.00 \\ 1.89 \\ 1.80 \end{array}$   | a)          | rui<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007  | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>2   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980   | (cell B)<br>-log(p/kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.62<br>3.53<br>3.45<br>3.37  | Image: point of the second system         Image: point of the second system<  | run I (cel        | l B)<br>g(p/kPa)<br>4.33<br>4.09<br>3.92<br>3.67<br>3.46<br>3.21<br>3.00<br>2.86<br>2.68<br>2.59  | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999  | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94  |
| ru           77K           962           973           983           993           1002           1012           1020           1030           1039           1049           1058           1067           1076   | $ \begin{array}{c} \text{m F2 (cell } C_2 \\ \hline -\log(p/\text{kP}) \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \\ 2.40 \\ 2.24 \\ 2.15 \\ 2.00 \\ 1.89 \\ 1.80 \\ \end{array} $  | a)          | rui<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007  | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>2   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980   | (cell B)<br>-log(p/kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37  | Image: Pa (1)         Image: T/K           908         917           931         947           962         978           991         1003           1014         1019   | run I (cel        | l B)<br>g(p/kPa)<br>4.33<br>4.09<br>3.92<br>3.67<br>3.46<br>3.21<br>3.00<br>2.86<br>2.68<br>2.59  | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999  | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94  |
| ru           77K           962           973           983           993           1002           1020           1030           1039           1049           1058           1067           1076  | $ \begin{array}{c} \text{m F2 (cell } C_2 \\ \hline -\log(p/\text{kP}) \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \\ 2.40 \\ 2.24 \\ 2.15 \\ 2.00 \\ 1.89 \\ 1.80 \\ \end{array} $  | <u>a</u> )  | гш<br>77К<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007   | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>2   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980   | (cell B)<br>-log(p/kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37<br>DI <sub>3</sub>   | Image: Pa (1)         Image: T/K           908         917           931         947           962         978           991         1003           1014         1019   | run I (cel        | l B)<br>g(p/kPa)<br>4.33<br>4.09<br>3.92<br>3.67<br>3.46<br>3.21<br>3.00<br>2.86<br>2.68<br>2.59  | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999  | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94  |
|   | m F2 (cell C <sub>2</sub><br>-log( <i>p</i> /kP<br>3.43<br>3.27<br>3.13<br>3.00<br>2.88<br>2.76<br>2.65<br>2.53<br>2.40<br>2.24<br>2.15<br>2.00<br>1.89<br>1.80<br>n A1 (cell C <sub>1</sub> )   | a)          | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007  | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>2<br>A2 (cell C  | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>TT<br>TT   | (cell B)<br>-log(p/kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37<br>ol <sub>3</sub><br>cell B)  | ru<br>Pa) T7/K<br>908<br>917<br>931<br>947<br>962<br>978<br>991<br>1003<br>1014<br>1019   | un I (cel         | l B)<br>g(p/kPa)<br>4.33<br>4.09<br>3.92<br>3.67<br>3.46<br>3.21<br>3.00<br>2.86<br>2.68<br>2.59  | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999  | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>D (cell A)  |
|   | $\frac{\text{m F2 (cell C_2)}}{-\log(p/\text{kP})}$ $\frac{-\log(p/\text{kP})}{3.43}$ $3.27$ $3.13$ $3.00$ $2.88$ $2.76$ $2.65$ $2.53$ $2.40$ $2.24$ $2.15$ $2.00$ $1.89$ $1.80$ $\frac{1}{1.80}$ $\frac{1}{1.80}$   | a)          | гил<br>77К<br>928<br>937<br>944<br>957<br>960<br>977<br>977<br>988<br>1000<br>1007<br>1007   | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>A2 (cell C<br>-log(p   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>Tr<br>T  | (cell B)<br>-log( <i>p</i> /kF<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37<br>bI <sub>3</sub><br>cell B)<br>-log( <i>p</i> /kF   | Image: red bit with the second seco | un I (cel<br>-log | I B)         g(p/kPa)         4.33         4.09         3.92         3.67         3.46         3.21         3.00         2.86         2.68         2.59 | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999<br>999<br>773<br>77K   | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>D (cell A)<br>-log(p/kPa)   |
| ги           77К           962           973           983           993           1002           1020           1030           1039           1049           1058           1066           1076           1076           1078           77К           871  | $\frac{\text{m F2 (cell C_2)}{-\log(p/\text{kP})}}{3.43}$ $3.27$ $3.13$ $3.00$ $2.88$ $2.76$ $2.65$ $2.53$ $2.40$ $2.24$ $2.15$ $2.00$ $1.89$ $1.80$ $1.41 (cell C_1)$ $-\log(p/\text{kPa})$ $4.55$  | a)          | ги<br>77К<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007<br>ГИК<br>971   | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>2<br>A2 (cell C<br>-log(p<br>2.5)  | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>TT<br>run B<br>77K<br>-<br>861   | (cell B)<br>-log( <i>p</i> /kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37<br>bI <sub>3</sub><br>cell B)<br>-log( <i>p</i> /kP<br>4.72   | Image: red with a state of the sta | un I (cel<br>-log | I B)         g(p/kPa)         4.33         4.09         3.92         3.67         3.46         3.21         3.00         2.86         2.68         2.59 | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999<br>999<br>999<br>77X<br>77K  | L (cell B)<br>-log( <i>p</i> /kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>D (cell A)<br>-log( <i>p</i> /kPa)<br>3.02   |
| ru           77K           962           973           983           993           1002           1020           1030           1039           1049           1058           1066           1076           1076           1088  | $\frac{\text{m F2 (cell C}_2}{-\log(p/\text{kP})}$ $\frac{3.43}{3.27}$ $3.13$ $3.00$ $2.88$ $2.76$ $2.65$ $2.53$ $2.40$ $2.24$ $2.15$ $2.00$ $1.89$ $1.80$ $\frac{1}{1.80}$ $\frac{1}{1.80}$ $\frac{1}{1.80}$  | a)          | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007<br>1007  | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>2<br>A2 (cell C<br>-log(p<br>-log(p<br>2.5<br>2.5)   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>Tri<br>run B<br>77K<br>-<br>861<br>879   | (cell B)<br>-log( <i>p</i> /kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37<br>bI <sub>3</sub><br>cell B)<br>-log( <i>p</i> /kP<br>4.72<br>4.48   | Image: Pair of the second system         Image: Pair of the seco   | un I (cel<br>-log | I B)         g(p/kPa)         4.33         4.09         3.92         3.67         3.46         3.21         3.00         2.86         2.68         2.59 | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999<br>999<br>999<br>77X<br>77K<br>955<br>971  | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>(cell A)<br>-log(p/kPa)<br>3.02<br>2.78   |
| ru           77K           962           973           983           993           1002           1020           1030           1039           1049           1058           1066           1076           1076           1088           run           77K           871           883           892  | $\begin{array}{c} \text{m F2 (cell } C_2 \\ \hline -\log(p/\text{kP} \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \\ 2.40 \\ 2.24 \\ 2.15 \\ 2.00 \\ 1.89 \\ 1.80 \\ \hline \text{n A1 (cell } C_1) \\ \hline -\log(p/\text{kPa} \\ 4.55 \\ 4.37 \\ 4.21 \\ \hline \end{array}$   | a)          | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007<br>1007  | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>TI<br>run B<br>77K<br>861<br>879<br>897  | (cell B)<br>-log( <i>p</i> /kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37<br>bI <sub>3</sub><br>cell B)<br>-log( <i>p</i> /kP<br>4.72<br>4.48<br>4.18   | Image: Pair of the second system         Image: Pair of the seco   | un I (cel<br>-log | I B)         g(p/kPa)         4.33         4.09         3.92         3.67         3.46         3.21         3.00         2.86         2.68         2.59 | run I<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999<br>999<br>999<br>773<br>981<br>990<br>999<br>999   | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>D (cell A)<br>-log(p/kPa)<br>3.02<br>2.78<br>2.54   |
| ru           77K           962           973           983           993           1002           1020           1030           1039           1049           1058           1067           1076           1088           run           77K           871           883           892           902           912   | $\frac{\text{m F2 (cell } C_2}{-\log(p/\text{kP})}$ $\frac{3.43}{3.27}$ $3.13$ $3.00$ $2.88$ $2.76$ $2.65$ $2.53$ $2.40$ $2.24$ $2.15$ $2.00$ $1.89$ $1.80$ $\frac{1}{1.80}$ $\frac{1}{1.80}$ $\frac{1}{1.80}$ $\frac{1}{1.80}$ $\frac{1}{1.80}$ $\frac{1}{1.80}$  | a)          | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007<br>700<br>77<br>77K<br>971<br>979<br>986<br>994  | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>T/<br>800<br>T/<br>K<br>-<br>861<br>879<br>897<br>913<br>920   | (cell B)<br>-log( <i>p</i> /kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37<br>bI <sub>3</sub><br>cell B)<br>-log( <i>p</i> /kP<br>4.72<br>4.48<br>4.18<br>3.91<br>2.64   | Image: Pair of the system         Image: Pair of the system           Pair of the system         908           917         931           947         962           978         991           1003         1014           1019         1019           mair of the system         972           983         990           9988         1905   | un I (cel<br>-log | I B)         g(p/kPa)         4.33         4.09         3.92         3.67         3.46         3.21         3.00         2.86         2.68         2.59 | run I<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999<br>999<br>999<br>773<br>981<br>990<br>999<br>999   | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>(cell A)<br>-log(p/kPa)<br>3.02<br>2.78<br>2.54<br>2.32<br>15   |
| ru           77K           962           973           983           993           1002           1020           1030           1039           1049           1058           1066           1076           1088              77K           871           883           892           902           912           922  | $\frac{\text{m F2 (cell } C_2}{-\log(p/\text{kP})}$ $\frac{3.43}{3.27}$ $3.13$ $3.00$ $2.88$ $2.76$ $2.65$ $2.53$ $2.40$ $2.24$ $2.15$ $2.00$ $1.89$ $1.80$ $\frac{1}{1.80}$  | a)          | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>977<br>988<br>1000<br>1007<br>1007<br>77K<br>971<br>979<br>986<br>994<br>994<br>971<br>979<br>986<br>994<br>001<br>008                       | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2  | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>T/<br>800<br>T/<br>K<br>-<br>861<br>879<br>897<br>913<br>929<br>940  | (cell B)<br>-log( <i>p</i> /kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37<br>bI <sub>3</sub><br>cell B)<br>-log( <i>p</i> /kP<br>4.72<br>4.48<br>4.18<br>3.91<br>3.64<br>3.47   | Image: red with a state of the sta | un I (cel<br>-log | I B)         g(p/kPa)         4.33         4.09         3.92         3.67         3.46         3.21         3.00         2.86         2.68         2.59 | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999<br>999<br>999<br>773<br>981<br>990<br>999<br>999<br>999  | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>D (cell A)<br>-log(p/kPa)<br>3.02<br>2.78<br>2.54<br>2.32<br>2.15<br>2.01   |
| ru           77K           962           973           983           993           1002           1020           1030           1039           1049           1058           1066           1076           1088              77K           871           883           892           902           912           922           930  | $\begin{array}{c} \text{m F2 (cell } C_2 \\ \hline -\log(p/\text{kP} \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \\ 2.40 \\ 2.24 \\ 2.15 \\ 2.00 \\ 1.89 \\ 1.80 \\ \hline \text{m A1 (cell } C_1) \\ \hline -\log(p/\text{kPa} \\ 4.55 \\ 4.37 \\ 4.21 \\ 4.04 \\ 3.88 \\ 3.73 \\ 3.62 \\ \hline \end{array}$   | a)          | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>977<br>988<br>1000<br>1007<br>1007<br>77K<br>971<br>979<br>986<br>994<br>001<br>008<br>0015  | n G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2<br>2   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.35<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65<br>.6  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>774<br>980<br>T/T<br>801<br>77K<br>861<br>879<br>897<br>913<br>929<br>940<br>948   | (cell B)<br>-log( <i>p</i> /kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37<br>bI <sub>3</sub><br>cell B)<br>-log( <i>p</i> /kP<br>4.72<br>4.48<br>4.18<br>3.91<br>3.64<br>3.47<br>3.37   | Image: red with a state of the sta | un I (cel<br>-log | I B)         g(p/kPa)         4.33         4.09         3.92         3.67         3.46         3.21         3.00         2.86         2.68         2.59 | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999<br>999<br>999<br>999<br>999<br>999<br>99   | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>D (cell A)<br>-log(p/kPa)<br>3.02<br>2.78<br>2.54<br>2.32<br>2.15<br>2.01<br>1.88   |
| ru           77K           962           973           983           993           1002           1020           1030           1039           1049           1058           1066           1076           1076           1078           871           883           892           902           912           930           939  | $\begin{array}{c} \text{m F2 (cell } C_2 \\ \hline -\log(p/\text{kP} \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \\ 2.40 \\ 2.24 \\ 2.15 \\ 2.00 \\ 1.89 \\ 1.80 \\ \hline \text{n A1 (cell } C_1) \\ \hline -\log(p/\text{kPa} \\ 4.55 \\ 4.37 \\ 4.21 \\ 4.04 \\ 3.88 \\ 3.73 \\ 3.62 \\ 3.47 \\ \hline \end{array}$   | a)          | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007<br>1007<br>77K<br>971<br>979<br>986<br>994<br>001<br>008<br>0015<br>022  | A2 (cell C<br>-log(p<br>A2 (cell C<br>-log(p<br>2.5<br>2.7<br>2.6<br>2.5<br>2.4<br>2.3<br>2.2  | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65   | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>774<br>980<br>774<br>980<br>774<br>980<br>774<br>980<br>897<br>913<br>929<br>913<br>929<br>940<br>948<br>959   | (cell B)<br>-log( <i>p</i> /kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37<br>bI <sub>3</sub><br>cell B)<br>-log( <i>p</i> /kP<br>4.72<br>4.48<br>4.18<br>3.91<br>3.64<br>3.47<br>3.7<br>3.16  | Image: Pair of the system         Im  | m C (cell         | I B)         g(p/kPa)         4.33         4.09         3.92         3.67         3.46         3.21         3.00         2.86         2.68         2.59 | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999<br>999<br>999<br>77K<br>77K<br>955<br>971<br>988<br>1004<br>1016<br>1027<br>1037<br>1043   | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>(cell A)<br>-log(p/kPa)<br>3.02<br>2.78<br>2.54<br>2.32<br>2.15<br>2.01<br>1.88<br>1.79   |
| ru           77K           962           973           983           993           1002           1020           1030           1039           1049           1058           1066           1076           1076           1078           871           883           892           902           912           922           930           939           948  | $\begin{array}{c} \text{m F2 (cell } C_2 \\ \hline -\log(p/\text{kP} \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \\ 2.40 \\ 2.24 \\ 2.15 \\ 2.00 \\ 1.89 \\ 1.80 \\ \hline \text{m A1 (cell } C_1) \\ \hline -\log(p/\text{kPa} \\ 4.55 \\ 4.37 \\ 4.21 \\ 4.04 \\ 3.88 \\ 3.73 \\ 3.62 \\ 3.47 \\ 3.33 \\ \hline \end{array}$   | a)          | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007<br>1007<br>77K<br>971<br>979<br>986<br>994<br>001<br>008<br>0015<br>022<br>029   | A2 (cell C<br>-log(p<br>A2 (cell C<br>-log(p<br>2.5<br>2.7<br>2.6<br>2.5<br>2.4<br>2.3<br>2.2<br>2.1   | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.65<br>.67<br>.81<br>.24<br>.66<br>.90<br>.81<br>.35<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65<br>.81<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>774<br>980<br>774<br>980<br>774<br>980<br>774<br>980<br>897<br>913<br>929<br>913<br>929<br>940<br>948<br>959<br>967  | (cell B)<br>-log( <i>p</i> /kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.62<br>3.53<br>3.45<br>3.37<br>bl <sub>3</sub><br>cell B)<br>-log( <i>p</i> /kP<br>4.72<br>4.48<br>4.18<br>3.91<br>3.64<br>3.47<br>3.7<br>3.16<br>3.04  | Image: Pair of the system         Image: Pair of the system           Pair of the system         908           917         931           947         962           978         978           991         1003           1014         1019           1013         1014           1019         972           983         990           9988         1005           1012         1019           1028         1036  | m C (cell         | I B)         g(p/kPa)         4.33         4.09         3.92         3.67         3.46         3.21         3.00         2.86         2.68         2.59 | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999<br>999<br>999<br>77K<br>77K<br>955<br>971<br>988<br>1004<br>1016<br>1027<br>1037<br>1043<br>1049                                 | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>(cell A)<br>-log(p/kPa)<br>3.02<br>2.78<br>2.54<br>2.32<br>2.15<br>2.01<br>1.88<br>1.79<br>1.69                                   |
| ru           77K           962           973           983           993           1002           1020           1030           1039           1049           1058           1066           1076           1076           1078           871           883           892           902           912           922           930           939           948           958           962  | $\begin{array}{c} \text{m F2 (cell } C_2 \\ \hline -\log(p/\text{kP} \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \\ 2.40 \\ 2.24 \\ 2.15 \\ 2.00 \\ 1.89 \\ 1.80 \\ \hline \text{m A1 (cell } C_1) \\ \hline -\log(p/\text{kPai} \\ 4.55 \\ 4.37 \\ 4.21 \\ 4.04 \\ 3.88 \\ 3.73 \\ 3.62 \\ 3.47 \\ 3.33 \\ 3.18 \\ 2.65 \\ \hline \end{array}$  | a)          | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007<br>1007<br>77K<br>971<br>979<br>986<br>994<br>001<br>008<br>0015<br>022<br>029<br>037                                    | A G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3  | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.35<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65<br>.6  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>TT<br>run B<br>77K<br>861<br>879<br>897<br>913<br>929<br>940<br>948<br>955<br>967<br>973<br>962  | (cell B)<br>-log( <i>p</i> /kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37<br>bI <sub>3</sub><br>cell B)<br>-log( <i>p</i> /kP<br>4.72<br>4.48<br>4.18<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.91<br>3.64<br>3.97<br>3.64<br>3.91<br>3.64<br>3.97<br>3.64<br>3.97<br>3.64<br>3.97<br>3.64<br>3.97<br>3.64<br>3.97<br>3.64<br>3.97<br>3.64<br>3.97<br>3.64<br>3.97<br>3.94<br>3.97<br>3.94<br>3.97<br>3.94<br>3.97<br>3.94<br>3.97<br>3.94<br>3.97<br>3.94<br>3.97<br>3.94<br>3.97<br>3.94<br>3.97<br>3.94<br>3.97<br>3.94<br>3.97<br>3.94<br>3.94<br>3.97<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3.94<br>3. | Image: red with a state of the sta | m C (cell         | I B)         g(p/kPa)         4.33         4.09         3.92         3.67         3.46         3.21         3.00         2.86         2.68         2.59 | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999<br>999<br>999<br>77K<br>955<br>971<br>988<br>1004<br>1016<br>1027<br>1037<br>1043<br>1049<br>1059                                | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>(cell A)<br>-log(p/kPa)<br>3.02<br>2.78<br>2.54<br>2.32<br>2.15<br>2.01<br>1.88<br>1.79<br>1.69<br>1.58<br>1.50                   |
| ru           77K           962           973           983           993           1002           1020           1020           1030           1039           1049           1058           1066           1088           Image: state stat | $\begin{array}{c} \text{m F2 (cell } C_2 \\ \hline -\log(p/\text{kP} \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \\ 2.40 \\ 2.24 \\ 2.15 \\ 2.00 \\ 1.89 \\ 1.80 \\ \hline \begin{array}{c} \text{n A1 (cell } C_1 \\ \hline -\log(p/\text{kPa} \\ 4.55 \\ 4.37 \\ 4.21 \\ 4.04 \\ 3.88 \\ 3.73 \\ 3.62 \\ 3.47 \\ 3.33 \\ 3.18 \\ 3.05 \\ 2.02 \\ \hline \end{array}$   | a)          | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007<br>1007<br>77K<br>971<br>979<br>986<br>994<br>001<br>008<br>0015<br>022<br>029<br>037<br>044<br>050                      | A2 (cell C<br>-log(p<br>A2 (cell C<br>-log(p<br>2.5<br>2.7<br>2.6<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.4<br>2.5<br>2.5<br>2.4<br>2.5<br>2.5<br>2.4<br>2.5<br>2.5<br>2.4<br>2.5<br>2.5<br>2.5<br>2.4<br>2.5<br>2.5<br>2.5<br>2.5<br>2.5<br>2.5<br>2.5<br>2.5 | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65   | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>TT<br>run B<br>77K<br>861<br>879<br>897<br>913<br>929<br>940<br>948<br>955<br>967<br>973<br>983<br>903   | (cell B)<br>-log(p/kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.62<br>3.53<br>3.45<br>3.37<br>bl <sub>3</sub><br>cell B)<br>-log(p/kP<br>4.72<br>4.48<br>4.18<br>3.91<br>3.64<br>3.47<br>3.7<br>3.16<br>3.04<br>2.94<br>2.82<br>2.66  | Image: red with a state of the sta | m C (cell         | I B)         g(p/kPa)         4.33         4.09         3.92         3.67         3.46         3.21         3.00         2.86         2.68         2.59 | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999<br>999<br>999<br>77K<br>955<br>971<br>988<br>1004<br>1016<br>1027<br>1037<br>1043<br>1049<br>1059<br>1066<br>1072                | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>(cell A)<br>-log(p/kPa)<br>3.02<br>2.78<br>2.54<br>2.32<br>2.15<br>2.01<br>1.88<br>1.79<br>1.69<br>1.58<br>1.50<br>1.41           |
| ru           77K           962           973           983           993           1002           1020           1020           1030           1039           1049           1058           1066           1088           0           7/1           871           883           892           902           912           922           930           948           958           966           973           980   | $\begin{array}{c} \text{m F2 (cell } C_2 \\ \hline -\log(p/\text{kP} \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \\ 2.40 \\ 2.24 \\ 2.15 \\ 2.00 \\ 1.89 \\ 1.80 \\ \hline \begin{array}{c} \text{n A1 (cell } C_1 \\ \hline -\log(p/\text{kPa} \\ 4.55 \\ 4.37 \\ 4.21 \\ 4.04 \\ 3.88 \\ 3.73 \\ 3.62 \\ 3.47 \\ 3.33 \\ 3.18 \\ 3.05 \\ 2.93 \\ 2.83 \\ \end{array}$  | a)<br>      | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007<br>1007<br>77K<br>971<br>979<br>986<br>994<br>001<br>008<br>0015<br>022<br>029<br>037<br>044<br>050<br>058               | A G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3  | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.27<br>.66<br>.90<br>.81<br>.27<br>.66<br>.90<br>.81<br>.27<br>.66<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65<br>.65   | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>Th<br>run B<br>77K<br>861<br>879<br>897<br>913<br>929<br>940<br>948<br>955<br>967<br>973<br>983<br>993<br>1003   | (cell B)<br>-log(p/kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37<br>bl <sub>3</sub><br>cell B)<br>-log(p/kP<br>4.72<br>4.48<br>4.18<br>3.91<br>3.64<br>3.47<br>3.76<br>3.04<br>2.94<br>2.82<br>2.66<br>2.54   | rt         rt           Pa)         77/K           908         917           931         947           962         978           978         991           1003         1014           1019         1019           972         983           990         998           1005         1012           1019         1028           1036         1043           1049         1057           1064         1057  | m C (cell         | I B)         g(p/kPa)         4.33         4.09         3.92         3.67         3.46         3.21         3.00         2.86         2.68         2.59 | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999<br>999<br>999<br>77K<br>77K<br>955<br>971<br>988<br>1004<br>1016<br>1027<br>1037<br>1043<br>1049<br>1059<br>1066<br>1072<br>1078 | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>D (cell A)<br>-log(p/kPa)<br>3.02<br>2.78<br>2.54<br>2.32<br>2.15<br>2.01<br>1.88<br>1.79<br>1.69<br>1.58<br>1.50<br>1.41<br>1.34 |
| ru           77K           962           973           983           993           1002           1020           1020           1030           1039           1049           1058           1066           1088           0           7/1           871           883           892           902           912           922           930           948           958           966           973           980           986   | $\begin{array}{c} \text{m F2 (cell } C_2 \\ \hline -\log(p/\text{kP} \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \\ 2.40 \\ 2.24 \\ 2.15 \\ 2.00 \\ 1.89 \\ 1.80 \\ \hline \begin{array}{c} \text{n A1 (cell } C_1 \\ \hline -\log(p/\text{kPa} \\ 4.55 \\ 4.37 \\ 4.21 \\ 4.04 \\ 3.88 \\ 3.73 \\ 3.62 \\ 3.47 \\ 3.33 \\ 3.18 \\ 3.05 \\ 2.93 \\ 2.83 \\ 2.74 \\ \end{array}$  | a)<br>      | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007<br>1007<br>77K<br>971<br>979<br>986<br>994<br>001<br>008<br>0015<br>022<br>029<br>037<br>044<br>050<br>058<br>064        | A G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3  | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.55<br>.55<br>.55<br>.24<br>.66<br>.90<br>.81<br>.55<br>.55<br>.55<br>.55<br>.55<br>.55<br>.55<br>.5  | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>774<br>980<br>774<br>861<br>879<br>897<br>913<br>929<br>940<br>948<br>959<br>967<br>973<br>983<br>993<br>1003  | (cell B)<br>-log(p/kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37<br>bl <sub>3</sub><br>cell B)<br>-log(p/kP<br>4.72<br>4.48<br>4.18<br>3.91<br>3.64<br>3.47<br>3.7<br>3.16<br>3.04<br>2.94<br>2.86<br>2.54  | rt         rt           Pa)         77K           908         917           931         947           962         978           978         991           1003         1014           1019         1019           77K         972           983         990           998         1005           1012         1019           1028         1036           1043         1049           1057         1064  | m C (cell         | I B)         g(p/kPa)         4.33         4.09         3.92         3.67         3.46         3.21         3.00         2.86         2.68         2.59 | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999<br>999<br>999<br>77K<br>955<br>971<br>988<br>1004<br>1016<br>1027<br>1037<br>1043<br>1049<br>1059<br>1066<br>1072<br>1078        | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>D (cell A)<br>-log(p/kPa)<br>3.02<br>2.78<br>2.54<br>2.32<br>2.15<br>2.01<br>1.88<br>1.79<br>1.69<br>1.58<br>1.50<br>1.41<br>1.34 |
| ru           77K           962           973           983           993           1002           1020           1020           1030           1039           1049           1058           1066           1088           0           77K           871           883           892           902           912           922           930           948           958           966           973           980           986           995   | $\begin{array}{c} \text{m F2 (cell } C_2 \\ \hline -\log(p/\text{kP} \\ 3.43 \\ 3.27 \\ 3.13 \\ 3.00 \\ 2.88 \\ 2.76 \\ 2.65 \\ 2.53 \\ 2.40 \\ 2.24 \\ 2.15 \\ 2.00 \\ 1.89 \\ 1.80 \\ \hline \begin{array}{c} \text{n A1 (cell } C_1 \\ \hline -\log(p/\text{kPa} \\ 4.55 \\ 4.37 \\ 4.21 \\ 4.04 \\ 3.88 \\ 3.73 \\ 3.62 \\ 3.47 \\ 3.33 \\ 3.18 \\ 3.05 \\ 2.93 \\ 2.83 \\ 2.74 \\ 2.62 \\ \hline \end{array}$   | a)<br>      | run<br>77K<br>928<br>937<br>944<br>957<br>960<br>977<br>988<br>1000<br>1007<br>1007<br>77K<br>971<br>979<br>986<br>994<br>001<br>008<br>0015<br>022<br>029<br>037<br>044<br>050<br>058<br>064<br>070 | A G (cell<br>-log<br>4<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3<br>3  | A)<br>(p/kPa)<br>.02<br>.86<br>.73<br>.56<br>.50<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.06<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.90<br>.81<br>.24<br>.66<br>.65<br>.67<br>.66<br>.90<br>.81<br>.27<br>.45<br>.66<br>.67<br>.47<br>.66<br>.67<br>.67<br>.67<br>.67<br>.67<br>.67<br>.6 | run H<br>77K<br>912<br>920<br>934<br>941<br>948<br>955<br>962<br>968<br>974<br>980<br>774<br>980<br>774<br>980<br>774<br>980<br>774<br>980<br>774<br>980<br>774<br>980<br>774<br>980<br>774<br>980<br>774<br>980<br>774<br>980<br>774<br>980<br>775<br>981<br>929<br>940<br>948<br>959<br>967<br>973<br>983<br>993<br>1003 | (cell B)<br>-log(p/kI<br>4.42<br>4.32<br>4.07<br>3.94<br>3.85<br>3.72<br>3.62<br>3.53<br>3.45<br>3.37<br>bl <sub>3</sub><br>cell B)<br>-log(p/kP<br>4.72<br>4.48<br>4.18<br>3.91<br>3.64<br>3.47<br>3.7<br>3.16<br>3.04<br>2.94<br>2.82<br>2.66<br>2.54  | rt           Pa)         77K           908         917           931         947           962         978           978         991           1003         1014           1019         1019           77K         972           983         990           998         1005           1012         1019           1028         1036           1043         1049           1057         1064   | m C (cell<br>-log | I B)         g(p/kPa)         4.33         4.09         3.92         3.67         3.46         3.21         3.00         2.86         2.68         2.59 | run 1<br>77K<br>921<br>934<br>939<br>945<br>955<br>964<br>973<br>981<br>990<br>999<br>999<br>77<br>77K<br>955<br>971<br>988<br>1004<br>1016<br>1027<br>1037<br>1043<br>1049<br>1059<br>1066<br>1072<br>1078         | L (cell B)<br>-log(p/kPa)<br>4.12<br>3.92<br>3.82<br>3.73<br>3.57<br>3.41<br>3.30<br>3.18<br>3.04<br>2.94<br>D (cell A)<br>-log(p/kPa)<br>3.02<br>2.78<br>2.54<br>2.32<br>2.15<br>2.01<br>1.88<br>1.79<br>1.69<br>1.58<br>1.50<br>1.41<br>1.34 |

| Table 4. (Continue |
|--------------------|
|--------------------|

|             |              |             |              | $TbI_3$     | (Continued)  |             |             |             |              |
|-------------|--------------|-------------|--------------|-------------|--------------|-------------|-------------|-------------|--------------|
| rur         | n E (cell B) | rur         | n F (cell B) | rur         | n G (cell A) | rui         | n H (cell B | rui         | n I (cell B) |
| <i>T</i> /K | -log(p/kPa)  | <i>T</i> /K | -log(p/kPa)  | <i>T</i> /K | -log(p/kPa)  | <i>T</i> /K | -log(p/kPa) | <i>T</i> /K | -log(p/kPa)  |
| 895         | 4.15         | 884         | 4.42         | 942         | 3.17         | 884         | 4.30        | 885         | 4.30         |
| 909         | 3.94         | 891         | 4.32         | 952         | 3.00         | 900         | 4.00        | 907         | 3.90         |
| 926         | 3.68         | 897         | 4.24         | 964         | 2.87         | 911         | 3.82        | 917         | 3.76         |
| 938         | 3.50         | 903         | 4.12         | 975         | 2.73         | 921         | 3.70        | 927         | 3.60         |
| 947         | 3.39         | 909         | 4.02         | 987         | 2.54         | 928         | 3.60        | 937         | 3.46         |
| 958         | 3.20         | 915         | 3.94         | 995         | 2.41         | 936         | 3.47        | 945         | 3.32         |
| 971         | 3.00         | 920         | 3.85         | 1003        | 2.30         | 944         | 3.35        | 953         | 3.22         |
| 980         | 2.86         | 927         | 3.74         | 1012        | 2.17         | 951         | 3.26        | 961         | 3.11         |
| 988         | 2.75         | 931         | 3.68         | 1020        | 2.04         | 959         | 3.13        | 967         | 3.01         |
| 998         | 2.60         | 935         | 3.62         | 1029        | 1.93         | 966         | 3.02        | 976         | 2.87         |
| 1006        | 2.51         | 940         | 3.55         | 1039        | 1.79         | 972         | 2.92        | 987         | 2.72         |
|             |              | 947         | 3.44         | 1049        | 1.65         | 977         | 2.85        | 998         | 2.56         |
|             |              | 953         | 3.35         | 1059        | 1.51         | 985         | 2.73        | 1009        | 2.42         |
|             |              | 963         | 3.18         | 1066        | 1.42         | 992         | 2.63        | 1018        | 2.30         |
|             |              | 973         | 3.02         |             |              | 998         | 2.55        | 1029        | 2.16         |
|             |              | 981         | 2.91         |             |              | 1004        | 2.47        |             |              |
|             |              | 988         | 2.81         |             |              | 1008        | 2.41        |             |              |
|             |              | 994         | 2.74         |             |              | 1013        | 2.35        |             |              |
|             |              | 1002        | 2.62         |             |              | 1017        | 2.28        |             |              |
|             |              | 1009        | 2.55         |             |              | 1021        | 2.21        |             |              |
|             |              |             |              |             |              | 1026        | 2.18        |             |              |



Figure 3. Experimental vapor pressure of  $TbCl_3$  (a),  $TbBr_3$  (b), and  $\alpha\text{-}TbI_3$  (c) measured by the torsion method.

temperatures, from the slopes of the selected equations (eqs 1-7). The enthalpies so obtained are reported in Table 7.

Table 5. Temperature Dependence of the Total Vapor Pressure of  $TbX_3$  (X = Cl, Br, I)

2.09

1033

|                                |       |     | no. of | $\Delta T$ | log(p/kPa) =                      | = A - B/(T/K)     |
|--------------------------------|-------|-----|--------|------------|-----------------------------------|-------------------|
| compd                          | cell  | run | points | K          | $A^a$                             | $B^{a}$           |
| TbCl <sub>3</sub> (l)          | В     | Α   | 15     | 942-1102   | $\textbf{8.87} \pm \textbf{0.04}$ | $11\ 828\pm45$    |
| TbCl <sub>3</sub> (l)          | В     | В   | 14     | 946-1075   | $9.41\pm0.10$                     | $12\;460\pm97$    |
| TbCl <sub>3</sub> (l)          | Α     | С   | 14     | 979-1091   | $\textbf{8.96} \pm \textbf{0.10}$ | $12~036\pm104$    |
| TbCl <sub>3</sub> (l)          | В     | Е   | 16     | 921-1037   | $9.37\pm0.16$                     | $12\;427\pm154$   |
| TbCl <sub>3</sub> (l)          | Α     | F   | 9      | 979-1067   | $9.20\pm0.20$                     | $12\;440\pm201$   |
| TbCl <sub>3</sub> (l)          | Α     | Н   | 13     | 976-1117   | $8.93 \pm 0.16$                   | $12\ 145\pm165$   |
| TbBr <sub>3</sub> (s)          | Α     | Α   | 14     | 957-1108   | $11.02\pm0.20$                    | $13\ 898\pm 202$  |
| TbBr <sub>3</sub> (s)          | Α     | В   | 15     | 922-1085   | $11.26\pm0.12$                    | $14\ 117 \pm 126$ |
| TbBr <sub>3</sub> (s)          | В     | С   | 11     | 904-960    | $10.62\pm0.18$                    | $13\ 496\pm 168$  |
| TbBr <sub>3</sub> (s)          | В     | D   | 10     | 915-975    | $11.25\pm0.26$                    | $14\ 241\pm 246$  |
| TbBr <sub>3</sub> (s)          | Α     | Е   | 14     | 920-1078   | $11.10\pm0.22$                    | $14~022\pm217$    |
| TbBr <sub>3</sub> (s)          | $C_1$ | F1  | 10     | 915 - 983  | $11.20\pm0.28$                    | $14\ 217\pm 262$  |
| TbBr <sub>3</sub> (s)          | $C_2$ | F2  | 14     | 962-1088   | $10.91\pm0.16$                    | $13\ 807\pm 165$  |
| TbBr <sub>3</sub> (s)          | Α     | G   | 9      | 928-1007   | $11.35\pm0.13$                    | $14\ 255\pm 128$  |
| TbBr <sub>3</sub> (s)          | В     | Н   | 10     | 912-980    | $11.04\pm0.18$                    | $14\ 107\pm 171$  |
| TbBr <sub>3</sub> (s)          | В     | I   | 10     | 908-1019   | $11.11\pm0.21$                    | $13~989\pm203$    |
| TbBr <sub>3</sub> (s)          | В     | L   | 10     | 921-999    | $11.24\pm0.16$                    | $14\ 146 \pm 151$ |
| $\alpha$ -TbI <sub>3</sub> (s) | $C_1$ | A1  | 15     | 871-995    | $11.02\pm0.11$                    | $13\ 591\pm 106$  |
| $\alpha$ -TbI <sub>3</sub> (s) | $C_2$ | A2  | 16     | 971-1077   | $12.07\pm0.12$                    | $14\ 630\pm 126$  |
| $\alpha$ -TbI <sub>3</sub> (s) | В     | В   | 13     | 861-1003   | $11.04\pm0.17$                    | $13\ 630\pm157$   |
| $\alpha$ -TbI <sub>3</sub> (s) | Α     | С   | 13     | 972-1064   | $11.70\pm0.26$                    | $14~075\pm266$    |
| $\alpha$ -TbI <sub>3</sub> (s) | Α     | D   | 13     | 955-1078   | $11.70\pm0.08$                    | $14~068\pm79$     |
| $\alpha$ -TbI <sub>3</sub> (s) | В     | Е   | 11     | 895-1006   | $10.93\pm0.17$                    | $13\ 520\pm 160$  |
| $\alpha$ -TbI <sub>3</sub> (s) | В     | F   | 20     | 884 - 1009 | $11.01\pm0.08$                    | $13\ 671\pm77$    |
| $\alpha$ -TbI <sub>3</sub> (s) | Α     | G   | 14     | 942 - 1066 | $11.96 \pm 0.18$                  | $14\ 280\pm183$   |
| $\alpha$ -TbI <sub>3</sub> (s) | В     | Н   | 22     | 884-1033   | $11.10\pm0.09$                    | $13\ 627\pm86$    |
| $\alpha$ -TbI <sub>3</sub> (s) | В     | Ι   | 15     | 885-1029   | $10.95\pm0.07$                    | $13\;492\pm62$    |

<sup>a</sup> The quoted errors are standard deviations.

**Gadolinium Trihalides.** The standard sublimation enthalpies of these compounds were obtained from their corresponding second-law values by the enthalpic increments,  $H^{\circ}(T) - H^{\circ}(298 \text{ K})$ , for the condensed and gaseous compounds selected by Pankratz.<sup>23</sup> The  $\Delta_{sub}H^{\circ}(298 \text{ K})$ values so obtained are reported in Table 7. As concerns GdBr<sub>3</sub>, considering the few experimental runs carried out above the molten compound, the final second-law standard sublimation enthalpy value,  $\Delta_{sub}H^{\circ}(298 \text{ K}) = 293 \text{ kJ}\cdot\text{mol}^{-1}$ with an estimated error of  $\pm 4 \text{ kJ}\cdot\text{mol}^{-1}$ , was evaluated giving a twin weight to the enthalpic value determined above the solid phase. The third-law standard sublimation enthalpies for gadolinium trihalides were also determined at some temperatures using the vapor pressure values

Table 6. Comparison of the Temperature Dependence of the Total Vapor Pressures of GdX<sub>3</sub> and TbX<sub>3</sub> (X = Cl, Br, I)

|                                    |           |               |               | $\Delta T$  | $\log(p/kPa) = A$  | $A - BK/T - C\log(T/K)$ |   |
|------------------------------------|-----------|---------------|---------------|-------------|--------------------|-------------------------|---|
| compd                              | ref       | method        | no. of points | K           | A                  | В                       | С |
| GdCl <sub>3</sub> (l) <sup>a</sup> | 10        | boiling point | 18            | 1369-1603   | 30.04              | 15 715                  | 6 |
| GdCl <sub>3</sub> (l)              | 11        | Knudsen       | 18            | 933-1073    | $8.23\pm0.30$      | $11\ 600 \pm 300$       |   |
| GdCl <sub>3</sub> (l)              | 9         | Knudsen       | 17            | 973 - 1044  | 10.10 <sup>b</sup> | 13 788 <sup>b</sup>     |   |
| GdCl <sub>3</sub> (l)              | this work | torsion       | 58            | 930-1213    | $9.50\pm0.30$      | $13\ 113\pm 300$        |   |
| GdBr <sub>3</sub> (s)              | 15        | mass-spectr   | 45            | 854-1020    | $11.093 \pm 0.050$ | $13\ 664\pm57$          |   |
| GdBr <sub>3</sub> (l)              | 16        | boiling point |               | 1220 - 1532 | $25.93 \pm 45$     | $13\ 603\pm97$          | 5 |
| GdBr <sub>3</sub> (l)              | 17        | static        | 41            | 1205 - 1621 | 7.97               | 10 384                  |   |
| $GdBr_3(s)$                        | this work | torsion       | 102           | 895-1057    | $11.46 \pm 0.20$   | $14~355\pm200$          |   |
| GdBr <sub>3</sub> (l)              | this work | torsion       | 32            | 1060-1179   | $9.75\pm0.30$      | $12\;671\pm400$         |   |
| GdI <sub>3</sub> (s)               | 19        | Knudsen       |               | 917-1025    | $13.56\pm0.28$     | $16~009\pm273$          |   |
| $\alpha$ -GdI <sub>3</sub> (s)     | this work | torsion       | 82            | 890-1012    | $10.99 \pm 0.20$   | $13~651\pm200$          |   |
| TbCl <sub>3</sub> (l) <sup>c</sup> | 10        | boiling point | 17            | 1326-1653   | 29.79              | 14 995                  | 6 |
| TbCl <sub>3</sub> (l)              | 9         | Knudsen       | 19            | 936 - 1044  | 9.37 <sup>b</sup>  | 12 777 <sup>b</sup>     |   |
| TbCl <sub>3</sub> (l)              | 13        | mass-spectr   | 60            | 890-1060    | $8.03 \pm 0.65$    | $11\ 678\pm261$         |   |
| TbCl <sub>3</sub> (l)              | 14        | mass-spectr   | 32            | 919 - 1054  | $8.32\pm0.63$      | $12\ 150\pm031$         |   |
| TbCl <sub>3</sub> (l)              | this work | torsion       | 81            | 921-1117    | $9.13\pm0.20$      | $12\ 210\pm 200$        |   |
| TbBr <sub>3</sub> (s)              | 15        | mass-spectr   | 46            | 836-1021    | $12.168 \pm 0.165$ | $14\ 607\pm 165$        |   |
| TbBr <sub>3</sub> (l)              | 16        | boiling point |               | 1219 - 1536 | $26.76 \pm 0.11$   | $13~349\pm72$           | 5 |
| TbBr <sub>3</sub> (s)              | this work | torsion       | 127           | 904 - 1108  | $11.09\pm0.20$     | $14~013\pm200$          |   |
| TbI <sub>3</sub> (s)               | 19        | Knudsen       |               | 889-995     | $11.71\pm0.25$     | $14\ 021\pm 231$        |   |
| $\alpha$ -TbI <sub>3</sub> (s)     | this work | torsion       | 152           | 861-1078    | $11.33\pm0.30$     | $13\ 850\pm400$         |   |

<sup>*a*</sup> Four Knudsen vapor pressure values were also reported by Moriarty<sup>8</sup> and drawn in Figure 3. <sup>*b*</sup> Equation obtained by us by treating with the least-squares method the experimental data reported in the Myers's paper.<sup>9</sup> <sup>*c*</sup> Four Knudsen vapor pressure values were also reported by Moriarty<sup>8</sup> and drawn in Figure 4.



**Figure 4.** Comparison of vapor pressures for (a)  $GdCl_3$ : ( $\bullet$ ) Moriarty;<sup>8</sup> (A) Myers;<sup>9</sup> (B) Dudchik;<sup>10</sup> (C) Evseeva;<sup>11</sup> (D) this work. (b)  $GdBr_3$ : (A) Gietmann;<sup>15</sup> (B) Makhmadmurodov;<sup>16</sup> (C) Weigel;<sup>17</sup> (D) this work. (c)  $GdI_3$ : (A) Hirayama;<sup>18</sup> (B) this work.



**Figure 5.** Comparison of vapor pressures for (a) TbCl<sub>3</sub>: ( $\bullet$ ) Moriarty;<sup>8</sup> (A) Myers;<sup>9</sup> (B) Dudchik;<sup>10</sup> (C) Khasanshin;<sup>13</sup> (D) this work. (b) TbBr<sub>3</sub>: (A) Gietmann;<sup>15</sup> (B) Makhmadmurodov;<sup>16</sup> (C) this work. (c) TbI<sub>3</sub>: (A) Hirayama;<sup>19</sup> (B) this work.

Table 7. Second- and Third-Law Sublimation Enthalpies in  $kJ \cdot mol^{-1}$  for GdX<sub>3</sub> and TbX<sub>3</sub> (X = Cl, Br, I)

|                                | Т    | secor  | third-law                                |  |
|--------------------------------|------|--|--|--|
| compd                          | K    | $\overline{\Delta_{\mathrm{sub},\mathrm{vap}}}H^{\mathrm{o}}(T)$ | $\Delta_{\rm sub}H^{\circ}(298~{\rm K})$ | $\Delta_{\rm sub}H^{\circ}(298~{\rm K})$ |
| GdCl <sub>3</sub> (l)          | 1071 | $251\pm 6$   | $317\pm 6$                               | $309\pm1$                                |
| GdBr <sub>3</sub> (s)          | 976  | $275\pm4$  | $289 \pm 4$                              | $292\pm1$                                |
| GdBr <sub>3</sub> (l)          | 1119 | $242\pm8$  | $301\pm8$                                | $295\pm1$                                |
| $\alpha$ -GdI <sub>3</sub> (s) | 951  | $261\pm4$  | $276\pm4$                                | $280 \pm 1$                              |
| TbCl <sub>3</sub> (l)          | 1019 | $234\pm4$  | $292\pm4$                                | $300\pm2$                                |
| TbBr <sub>3</sub> (s)          | 1006 | $268 \pm 4$  | $285\pm4$                                | $292 \pm 2,^{a} 287 \pm 2^{b}$           |
| $\alpha$ -TbI <sub>3</sub> (s) | 970  | $265\pm4$  | $282\pm4$                                | $277\pm2$                                |

<sup>*a*</sup> Values obtained using for TbBr<sub>3</sub>(g) the free energy function reported by Pankratz.<sup>23</sup> <sup>*b*</sup> Values obtained using for TbBr<sub>3</sub>(g) the free energy function reported by Gietmann.<sup>15</sup>

calculated by the selected eqs 1-4 and the corresponding free energy functions (fef),  $[G^{\circ}(T) - H^{\circ}(298 \text{ K})]/T$ , reported in Pankratz's Tables.<sup>23</sup> The results are reported in Table 8. The third-law  $\Delta_{sub}H^{\circ}(298 \text{ K})$  values so obtained do not present evident temperature trends and are decidedly in good agreement with the corresponding second-law enthalpies (see Table 7). The difference of about 2 kJ·mol<sup>-1</sup> between the third-law  $\Delta_{sub}H^{\circ}(298 \text{ K})$  values for GdBr<sub>3</sub> determined by using the vapor pressures measured above molten and solid compounds (see Table 8) can be mainly due to a very small shift of the pressure data connected mainly with errors in the cell constants of cell C. Incidentally, this shift can also be the cause of the lower values of the melting point determined from the intersection of the log versus 1/T straight lines (see Table 3) than the selected one.<sup>22</sup> In any case, the vapor pressures measured above the solid compound were considered more reliable in view of the agreement of the pressure values determined by using several cells B and of the higher number of experimental points compared to those measured above the liquid phase.

On this basis we propose the following standard sublimation enthalpies,  $\Delta_{sub}H^{\circ}(298 \text{ K}) = (311 \pm 4)$ ,  $(292 \pm 2)$ , and  $(279 \pm 2) \text{ kJ} \cdot \text{mol}^{-1}$  for GdCl<sub>3</sub>, GdBr<sub>3</sub>, and GdI<sub>3</sub>, respectively. Our  $\Delta_{sub}H^{\circ}(298 \text{ K})$  value for GdCl<sub>3</sub> agrees with that mass-spectrometrically determined, from the slope of a log(I<sup>+</sup>T) versus 1/*T* equation, by Ciach et al.<sup>12</sup> [(298 ± 17) kJ·mol<sup>-1</sup>] and that obtained by Myers and Hannay <sup>9</sup> [(311 ± 12) kJ·mol<sup>-1</sup>] from Knudsen measurements. Decidedly lower is the Knudsen enthalpy value reported by Evseeva and Zenkevich<sup>11</sup> [ $\Delta_{sub}H^{\circ}(1003 \text{ K}) = (222 \pm 11)$  kJ·mol<sup>-1</sup>]. As concerns GdBr<sub>3</sub>, our selected enthalpy value is slightly higher than that selected by Gietmann,<sup>15</sup>  $\Delta_{sub}H^{\circ}$ (298 K) = (280.2 ± 12.5) kJ·mol<sup>-1</sup>. Our sublimation enthalpy found for  $\alpha$ -GdI<sub>3</sub> is lower than those reported by Hirayama et al. [(295 ± 2) kJ·mol<sup>-1</sup> (ref 18) and 321 ± 5 kJ·mol<sup>-1</sup> (ref 19)].

Terbium Trihalides. From the second-law sublimation enthalpies for these compounds reported in Table 7, the corresponding standard values were obtained using the enthalpic increments selected by Pankratz.<sup>23</sup> The enthalpic increment for TbBr<sub>3</sub>(s) was evaluated by the expression of the temperature dependence of the heat capacity,  $c_{\rm p} = (94.6$ +  $(1.84 \times 10^{-2})$  T/K) J·mol<sup>-1</sup>, proposed by Myers and Graves.<sup>24</sup> The so obtained second-law  $\Delta_{sub} H^{\circ}(298 \text{ K})$  values of terbium trihalides are also reported in Table 7. The third-law values of these enthalpies were also calculated by using the vapor pressures derived from eqs 5-7 at some temperatures and the corresponding fef selected by Pankratz.<sup>23</sup> In absence in Pankratz's Tables of thermodynamic data for TbBr<sub>3</sub>(s), the fef of this compound were evaluated using the standard entropy reported by Gietmann et al.,<sup>15</sup>  $S^{\circ}(298 \text{ K}) = 194 \text{ J} \cdot \text{mol}^{-1} \cdot \text{K}^{-1}$ , and the heat capacity above-mentioned. The third-law sublimation enthalpies so obtained for all compounds present decidedly negligible temperature trends (see Table 8), and their average values may be considered in agreement with the corresponding second-law ones. On this basis we propose as standard sublimation enthalpy for TbCl<sub>3</sub> the value  $\Delta_{sub}H^{\circ}(298 \text{ K}) = 296 \text{ kJ} \cdot \text{mol}^{-1}$ , the average of the secondand third-law results, with an estimated error of  $\pm 4$ kJ·mol<sup>-1</sup>. This value agrees within the errors with those determined by Myers and Hannay,<sup>9</sup> (303  $\pm$  13) kJ·mol<sup>-1</sup>, and by Kudin et al.,<sup>14</sup> (290  $\pm$  6) kJ·mol<sup>-1</sup>. The massspectrometric value obtained by Khasanshin et al.<sup>13</sup> [(280

Table 8. Third-Law Sublimation Enthalpies for GdX<sub>3</sub> and TbX<sub>3</sub> (X = Cl, Br, I)

|                                | T                 | р                   | $-R\ln(p/\text{atm})$           | $-\Delta$ (fef)                        | Δ <i>H</i> °(298 K)                    |
|--------------------------------|-------------------|---------------------|---------------------------------|--|--|
| compd                          | K                 | kPa                 | $J \cdot mol^{-1} \cdot K^{-1}$ | $J \cdot mol^{-1} \cdot K^{-1}$        | kJ∙mol <sup>−1</sup>                   |
| GdCl <sub>3</sub> (l)          | 900               | $8.45	imes10^{-6}$  | 135.5                           | 208.7                                  | 309.8                                  |
| GdCl <sub>3</sub> (l)          | 1000              | $2.42	imes10^{-4}$  | 107.6                           | 202.1                                  | 309.7                                  |
| GdCl <sub>3</sub> (l)          | 1100              | $3.77	imes10^{-3}$  | 84.8                            | 196.2                                  | 309.1                                  |
| GdCl <sub>3</sub> (l)          | 1200              | $3.71	imes10^{-2}$  | 65.8                            | 190.8                                  | 307.9                                  |
| GdBr <sub>3</sub> (s)          | 900               | $3.27	imes10^{-5}$  | 124.2                           | 200.2                                  | 292.0                                  |
| GdBr <sub>3</sub> (s)          | 1000              | $1.29	imes10^{-3}$  | 93.7                            | 198.7                                  | 292.4                                  |
| GdBr <sub>3</sub> (s)          | 1058              | $7.87	imes10^{-3}$  | 78.7                            | 197.8                                  | 292.5                                  |
| GdBr <sub>3</sub> (l)          | 1058              | $5.94	imes10^{-3}$  | 81.0                            | 197.8                                  | 295.0                                  |
| GdBr <sub>3</sub> (l)          | 1100              | $1.70	imes10^{-2}$  | 72.2                            | 195.8                                  | 294.9                                  |
| GdBr <sub>3</sub> (l)          | 1200              | $1.55	imes10^{-1}$  | 53.9                            | 191.3                                  | 294.2                                  |
| $\alpha$ -GdI <sub>3</sub> (s) | 900               | $6.57	imes10^{-5}$  | 118.4                           | 192.2                                  | 279.6                                  |
| $\alpha$ -GdI <sub>3</sub> (s) | 950               | $4.13	imes 10^{-4}$ | 103.2                           | 191.4                                  | 279.8                                  |
| $\alpha$ -GdI <sub>3</sub> (s) | 1000              | $2.16	imes10^{-3}$  | 89.4                            | 190.6                                  | 280.0                                  |
| $\alpha$ -GdI <sub>3</sub> (s) | 1013 <sup>c</sup> | $3.23	imes10^{-3}$  | 86.1                            | 190.4                                  | 280.1                                  |
| TbCl <sub>3</sub> (l)          | 900               | $3.62	imes10^{-5}$  | 123.4                           | 208.5                                  | 298.7                                  |
| TbCl <sub>3</sub> (l)          | 1000              | $8.23	imes10^{-4}$  | 97.4                            | 202.5                                  | 299.9                                  |
| TbCl <sub>3</sub> (l)          | 1100              | $1.06	imes10^{-2}$  | 76.2                            | 197.1                                  | 300.6                                  |
| TbBr <sub>3</sub> (s)          | 900               | $3.32	imes10^{-5}$  | 124.1                           | 199.1, <sup>a</sup> 194.1 <sup>b</sup> | 290.9, <sup>a</sup> 286.4 <sup>b</sup> |
| TbBr <sub>3</sub> (s)          | 1000              | $1.20	imes10^{-3}$  | 94.3                            | 197.5, <sup>a</sup> 192.8 <sup>b</sup> | 291.8, <sup>a</sup> 287.2 <sup>b</sup> |
| TbBr <sub>3</sub> (s)          | 1100              | $2.25	imes10^{-2}$  | 69.9                            | 195.9, <sup>a</sup> 191.2 <sup>b</sup> | 292.4, <sup>a</sup> 287.3 <sup>b</sup> |
| $\alpha$ -TbI <sub>3</sub> (s) | 800               | $1.05	imes10^{-6}$  | 152.8                           | 193.5                                  | 277.1                                  |
| $\alpha$ -TbI <sub>3</sub> (s) | 900               | $8.78	imes10^{-5}$  | 116.0                           | 191.8                                  | 277.0                                  |
| $\alpha$ -TbI <sub>3</sub> (s) | 1000              | $3.04	imes10^{-3}$  | 86.6                            | 190.1                                  | 276.7                                  |
| $\alpha$ -TbI <sub>3</sub> (s) | $1080^{d}$        | $3.22	imes10^{-2}$  | 66.9                            | 188.7                                  | 276.1                                  |

<sup>*a*</sup> Values obtained using the free energy function for TbBr<sub>3</sub>(g) reported by Pankratz.<sup>23</sup> <sup>*b*</sup> Values obtained using the free energy function for TbBr<sub>3</sub>(g) reported by Gietmann.<sup>15</sup> <sup>*c*</sup> Solid  $\alpha - \beta$  transition for GdI<sub>3</sub>(s) <sup>*d*</sup> Solid  $\alpha - \beta$  transition for TbI<sub>3</sub>(s)

 $\pm$  5) kJ·mol<sup>-1</sup>] is slightly more low. Two third-law  $\Delta_{sub}H^{\circ}$ -(298 K) values were calculated for TbBr<sub>3</sub>: one, (287  $\pm$  2) kJ·mol<sup>-1</sup>, using for the gaseous compound the fef proposed by Gietmann et al.  $^{15}$  and another one, (292  $\pm$  2) kJ·mol  $^{-1}$ , using the fef selected by Pankratz<sup>23</sup> (see Table 8). The first value is in better agreement with the second-law one [(285  $\pm$  4) kJ·mol<sup>-1</sup>], so that we propose as sublimation enthalpy for TbBr<sub>3</sub> the average value of 288 kJ·mol<sup>-1</sup> with an overestimated error of  $\pm 4 \text{ kJ} \cdot \text{mol}^{-1}$ . This enthalpic value is practically coincident with that proposed by Gietmann<sup>15</sup>  $[(288.9 \pm 6.3) \text{ kJ} \cdot \text{mol}^{-1}]$  obtained as the average of the corresponding second- and third-law values [(294.3  $\pm$  7.8) and  $(279.1 \pm 10.5)$  kJ·mol<sup>-1</sup>, respectively]. As concerns the results obtained from second- and third-law treatment of the vapor pressures for  $\alpha$ -TbI<sub>3</sub>, they are in satisfactory agreement, so that we propose as final standard sublimation enthalpy the average of their values,  $\Delta_{sub} H^{\circ}(298 \text{ K}) =$ 279 kJ·mol<sup>-1</sup>, with an estimated error limit of  $\pm 2$  kJ·mol<sup>-1</sup>. This value, equal to that found in the present work for  $\alpha$ -GdI<sub>3</sub>, agrees with the value [(284 ± 5) kJ·mol<sup>-1</sup>] reported by Hirayama et al.<sup>19</sup>

## Conclusion

In the present work, the total vapor pressures of gadolinium and terbium trihalides were measured by the torsion-effusion method. As the contribution of partial pressures of the dimer forms should be negligible, in any case of the same order of magnitude of the uncertainties associated with the measured pressure values, the experimental pressure data were treated as partial pressures of the monomeric forms. The selected eqs 1-7 represent the best fit of the temperature dependence of these pressures. By second- and third-law treatment of the vapor pressure data represented by these equations, the standard sublimation enthalpies of these halides were calculated. The selected final values,  $\Delta_{sub}H^{\circ}(298 \text{ K}) = (311 \pm 4)$ ,  $(292 \pm 2)$ , and (279  $\pm$  2)  $kJ{\cdot}mol^{-1}$  for  $GdCl_3\text{,}$   $GdBr_3\text{,}$  and  $\alpha\text{-}GdI_3\text{,}$ respectively, present, as observed for the previously studied trihalides of the first lanthanides, a decreasing trend going from trichlorides to triiodides. This trend is also present, but smoother, in the sublimation enthalpies for terbium trihalides,  $\Delta_{sub}H^{\circ}(298 \text{ K}) = (296 \pm 4)$ ,  $(288 \pm 4)$ , and  $(279 \pm 4)$  $\pm$  2) kJ·mol<sup>-1</sup> for TbCl<sub>3</sub>, TbBr<sub>3</sub>, and  $\alpha$ -TbI<sub>3</sub>, respectively.

## **Literature Cited**

- Brunetti, B.; Villani, A. R.; Piacente, V.; Scardala, P. Vaporization Studies of Lanthanum Trichloride, Tribromide, and Triiodide. J. Chem. Eng. Data 2000, 45, 231-236.
- Villani, A. R.; Brunetti, B.; Piacente, V. Vapor Pressure and Enthalpies of Vaporization of Cerium Trichloride, Tribromide and Triiodide. J. Chem. Eng. Data 2000, 45, 823-828.
- (3) Villani, A. R.; Brunetti, B.; Piacente, V. Vapor Pressures and Sublimation Enthalpies of Praseodymium Trichloride, Tribromide, and Triiodide. J. Chem. Eng. Data 2000, 45, 1167-1172.

- (4) Villani, A. R.; Scardala, P.; Brunetti, B; Piacente, V. Sublimation Enthalpies of Neodymium Trichloride, Tribromide and Triiodide from Torsion Vapor Pressure Measurements. J. Chem. Eng. Data 2002, 47 (3), 428-434.
- Scardala, P.; Villani, A. R.; Brunetti, B.; Piacente, V. Vaporization Study of Samarium Trichloride, Samarium Tribromide and Samarium Diiodide. *Mater. Chem. Phys.* **2003**, *78*, 637–644.
- Brunetti, B.; Vassallo, P.; Piacente, V.; Scardala, P. Vaporization Studies of Dysprosium Trichloride, Tribromide, and Triiodide. J. *Chem. Eng. Data* **1999**, *44*, 509–515. Piacente, V.; Brunetti, B.; Scardala, P.; Villani, A. R. Vapor
- Pressure and Sublimation Enthalpies of Holmium Trichloride, Tribromide, and, Triiodide. J. Chem. Eng. Data 2002, 47, 388 396
- Moriarty, J. L. Vapor Pressures of Yttrium and Rare Earth Chlorides above Their Melting Points. J. Chem. Eng. Data **1963**, (8) 8.422 - 424
- Myers, C. E.; Hannay, M. H. Vapor Pressures and Sublimation Thermodynamics of GdCl<sub>3</sub>, TbCl<sub>3</sub> and DyCl<sub>3</sub>. J. Less-Common Met. 1980, 70, 15-24.
- (10) Dudchik, G. P.; Polyachenok, O. G.; Novikov, G. I. Saturated Vapor Pressures of Yttrium, Praseodymium, Gadolinium, Terbium and Dysprosium Chlorides. Russ. J. Inorg. Chem. 1969, 14, 1669-1670.
- (11) Evseeva, G. V.; Zenkevich, L. V. Determination of the Vapor Pressure of Gadolinium Chloride. Vestn. Mosk. Univ., Khim. 1978, 33, 89-91.
- (12) Ciach, S.; Nicholson, A. J. C.; Swingler, D. L.; Thistlethwaite, P. J. Mass Spectrometric Study of the Vapor Phase over Neodymium Chloride and Gadolinium Chloride. Inorg. Chem. 1973, 12, 2072-2074.
- (13) Khasanshin, I. V.; Kudin, L. S.; Pogrebnoi, A. M. A Mass Spectrometric Study of Saturated Vapor Over Terbium Trichloride and TbCl3-DyČl3 System. Russ. J. Phys. Chem. 1999, 73, 849 - 855.
- (14) Kudin, L. S.; Pogrebnoi, A. M.; Khasanshin, I. V.; Motalor, V. B. Thermodynamic Properties of Neutral and Charged Species in High-Temperature Vapor Over Terbium and Thulium Trichlorides. High Temp. Sci. 2000, 32, 557-565.
- (15) Gietmann, C.; Hilpert, K.; Nickel, H. Thermodynamic Properties of Rare Earth Bromides. *Ber. Forschungszent.* **1997**, 1–171. (16) Makhmadmurodov, A.; Temurova, M.; Sharipov, A. Thermody
- namics of Vaporization of Rare Earth Bromides. Izv. Akad. Nauk
- Tadzh. SSR. Otd. Fiz.-Mat. Geol.-Khim. Nauk 1989, 1, 39–42.
  (17) Weigel, V. F.; Trinkl, G. The vapour Pressure for Gadolinium Tribromide by the Cup Method of W. Fischer. Z. Anorg. Allg. Chem. 1970, 377, 228–239.
  (18) Hirayama, C.; Castle, P. M. Mass Spectra of Rare Earth Triio-dides. J. Phys. Chem 1973, 77, 3110–3114.
- dides. J. Phys. Chem. 1973, 77, 3110–3114. Hirayama, C.; Rome, J. F.; Camp, F. E. Vapor Pressures and
- Thermodynamic of Lanthanide Triiodides. J. Chem. Eng. Data **1975**. 20. 1-6.
- (20) Piacente, V.; Fontana, D.; Scardala, P. Enthalpies of Vaporization of a Homologous Series of n-Alkanes Determined from Vapor
- Pressure Measurements. J. Chem. Eng. Data 1994, 39, 231–237.
  (21) Hultgren, R.; Desai, P. D.; Hawkins, D. T.; Gleiser, M.; Kelley, K. K.; Wagman, D. D. Selected Values of the Thermodynamic Properties of the Elements; American Society for Metals: Metals Park, OH, 1973.
- (22) Dworkin, A. S.; Bredig, M. A. Enthalpy of Lanthanide Chlorides, Bromides, and Iodides from 298 to 1300 K: Enthalpies of Fusion and Transition. High Temp. Sci. 1971, 3, 81-90.
- (23)Pankratz, L. B. Thermodynamic Properties of Halides; Bull. U. S. Department Int., Bureau of Mines 674; Washington, DC, 1984.
- (24) Myers, C. E.; Graves, D. T. Vaporization Thermodynamics of Lanthanide Trihalides. J. Chem. Eng. Data 1977, 22, 440-445.

Received for review October 2, 2002. Accepted January 6, 2003.

JE020189P